

# **DWA-IWAMA-2<sup>nd</sup> International Capacity Development Workshop „Energy Production in WWT“**

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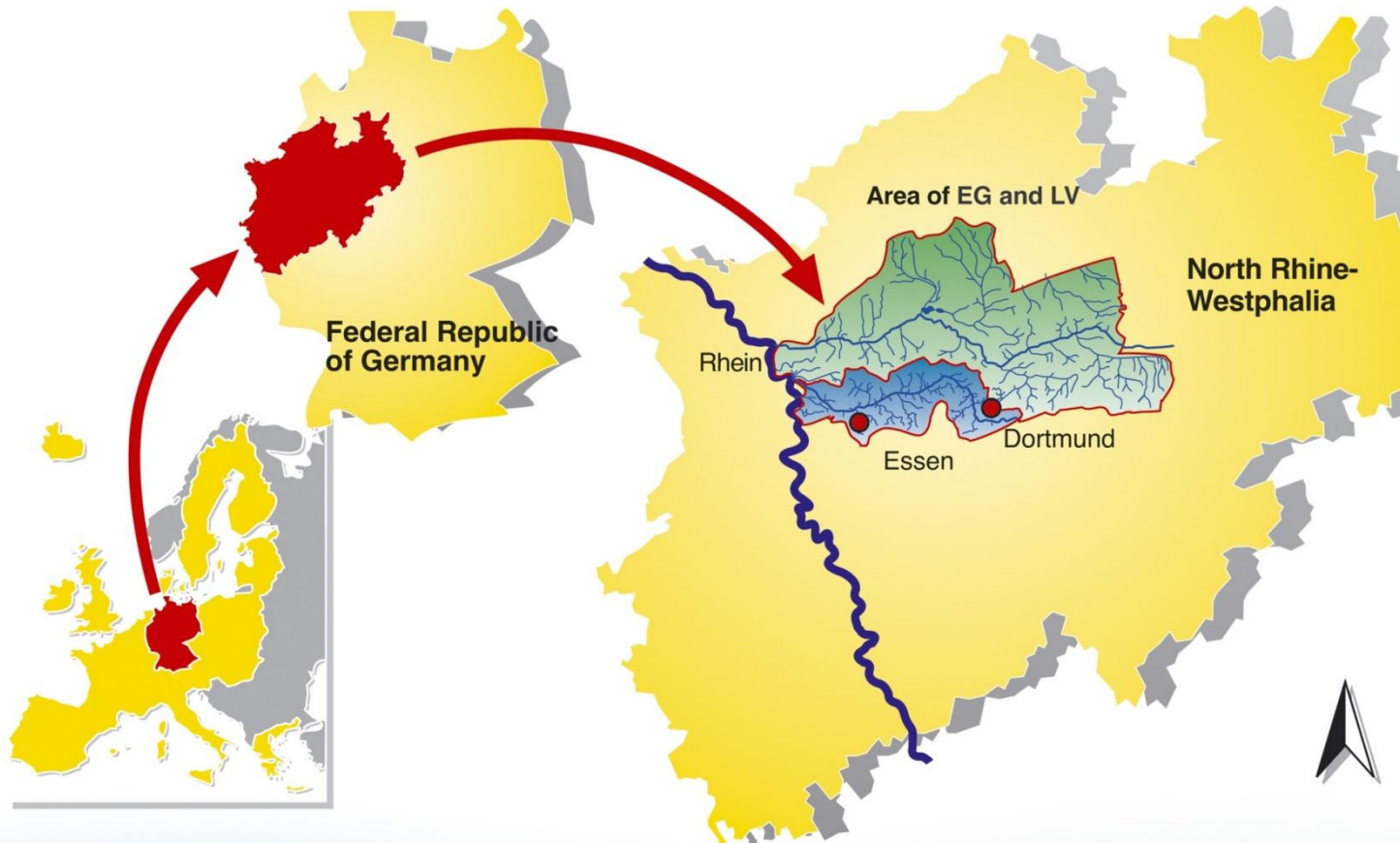
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## CV – Personal Details

- Karl-Georg Schmelz
- 56 years, married, 3 Kids
- Since 1990 working for Emschergenossenschaft and Lippeverband
- Misc. working areas, currently in the R&D departement, responsible for sewage sludge and industrial wastewater
- Member of different specialist groups of the DWA (i.a. DWA KEK 1.6: Sewage Sludge Disintegration“)
- Education of WWTP-operators and students at the University Duisburg-Essen

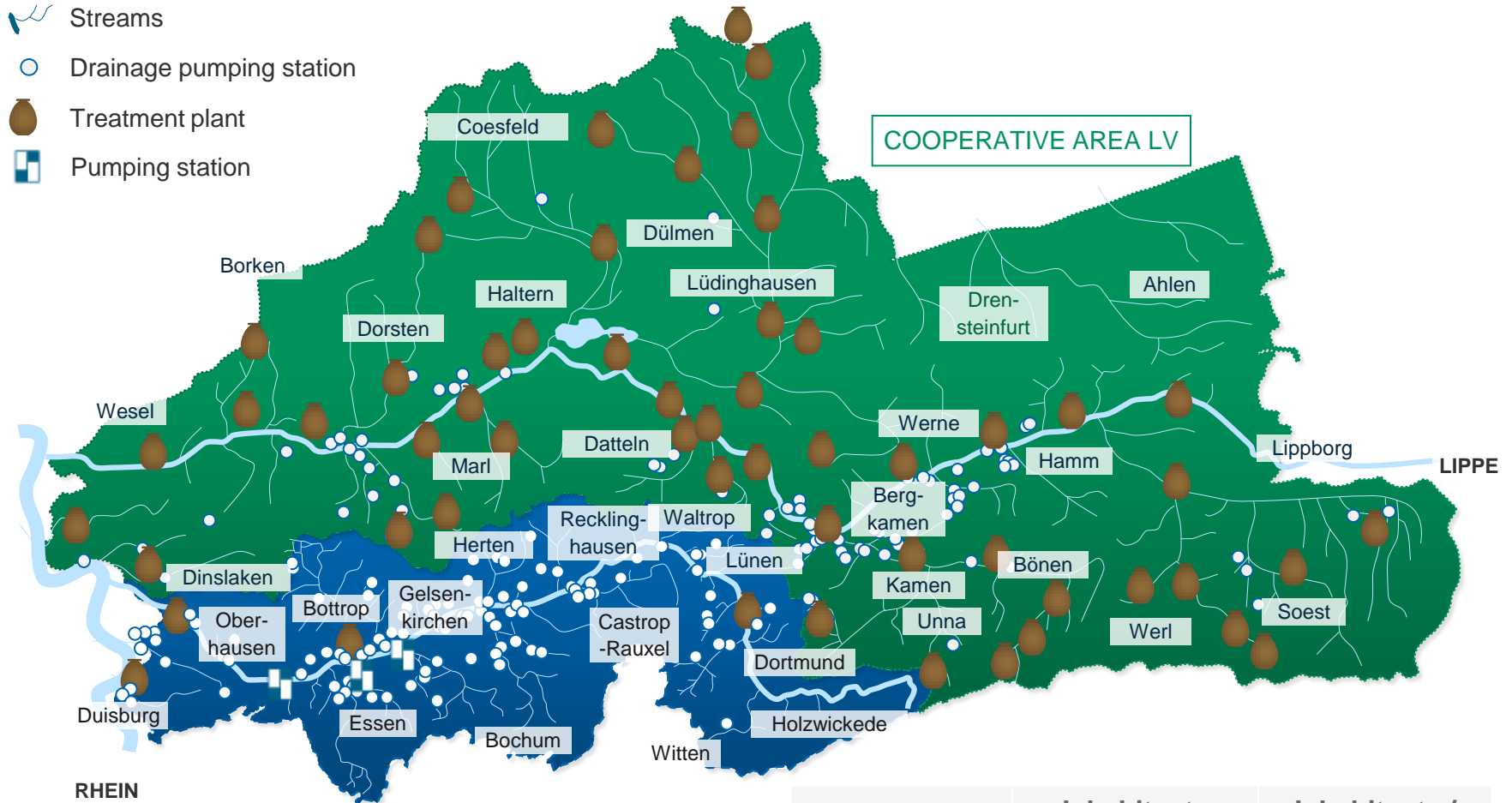


# Operating Area EG/LV



EMSCHER LIPPE

# Our catchment area



	Area (km <sup>2</sup> )	Inhabitants (mill.)	Inhabitants / km <sup>2</sup>
Lippeverband	3,280	1.4	427
Emschergenossenschaft	865	2.2	2,546

# Sewage Sludge Disintegration

## DWA-Specialist Group KEK 1.6

- **Merkblatt DWA-M 302 (guidelines)**
  - Published in December 2016
- **Specialist group is working since 1996**
  - 6 working documents
- **Members:**
  - Müller-Schaper, Johannes (Speaker)
  - Bormann, Hinnerk
  - Heinzmann, Bernd
  - Kopplow, Ole
  - Oles, Jürgen
  - Rand, Wiebke
  - Schmelz, Karl-Georg
  - Seiler, Kainan
  - Wagenbach, Anja

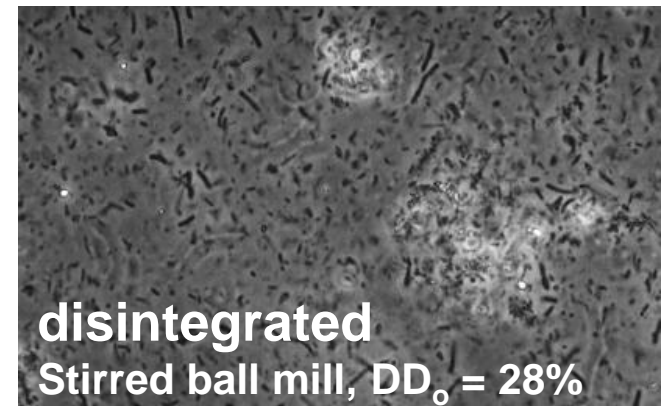
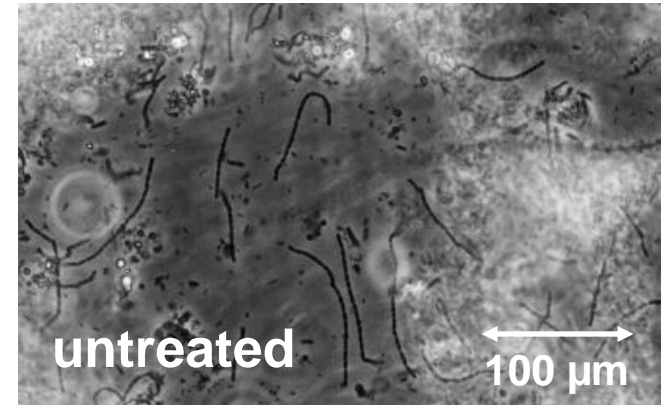
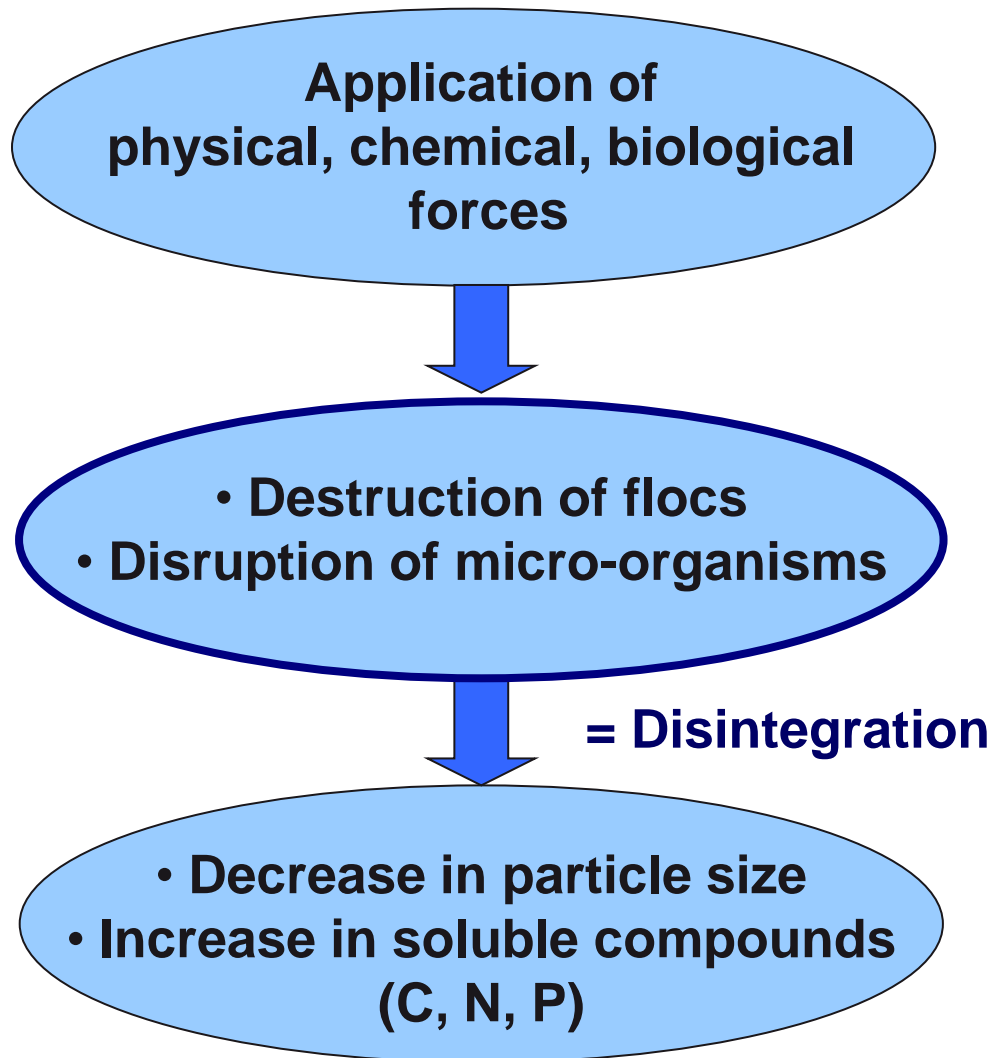




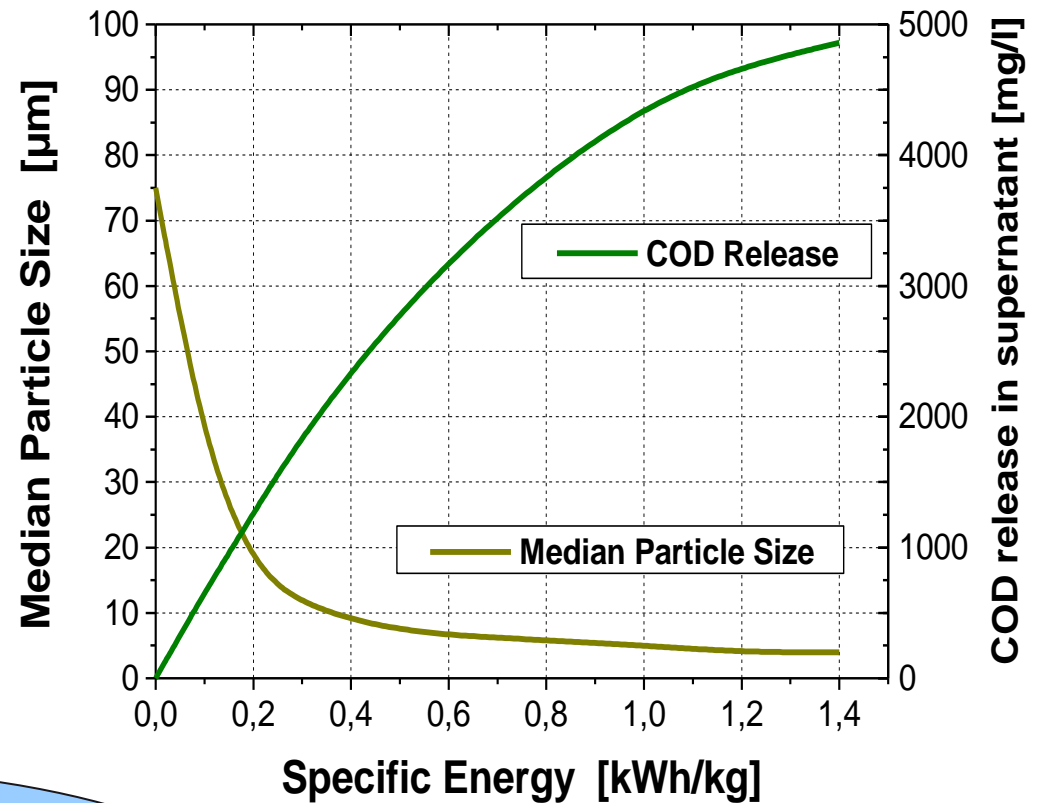
# Definition of Sewage Sludge Disintegration

- **Disintegration** of sewage sludge through the **impact of external forces** (physical, chemical, biological)
- **Degree of disintegration** depends on used procedure, energy input and characteristics of sludge
  - Disintegration of flocs (reduction of particle size, destruction of microorganism chains;  $< 0,1 \text{ kWh/ kg DS}$ )
  - Disintegration of cells ( $> 0,25 \text{ kWh/kg DS}$ )
- **Objectives:**
  - Increase bioavailability of the organic carbon
  - improvement of the sludge characteristics

# Disintegration of sewage sludge

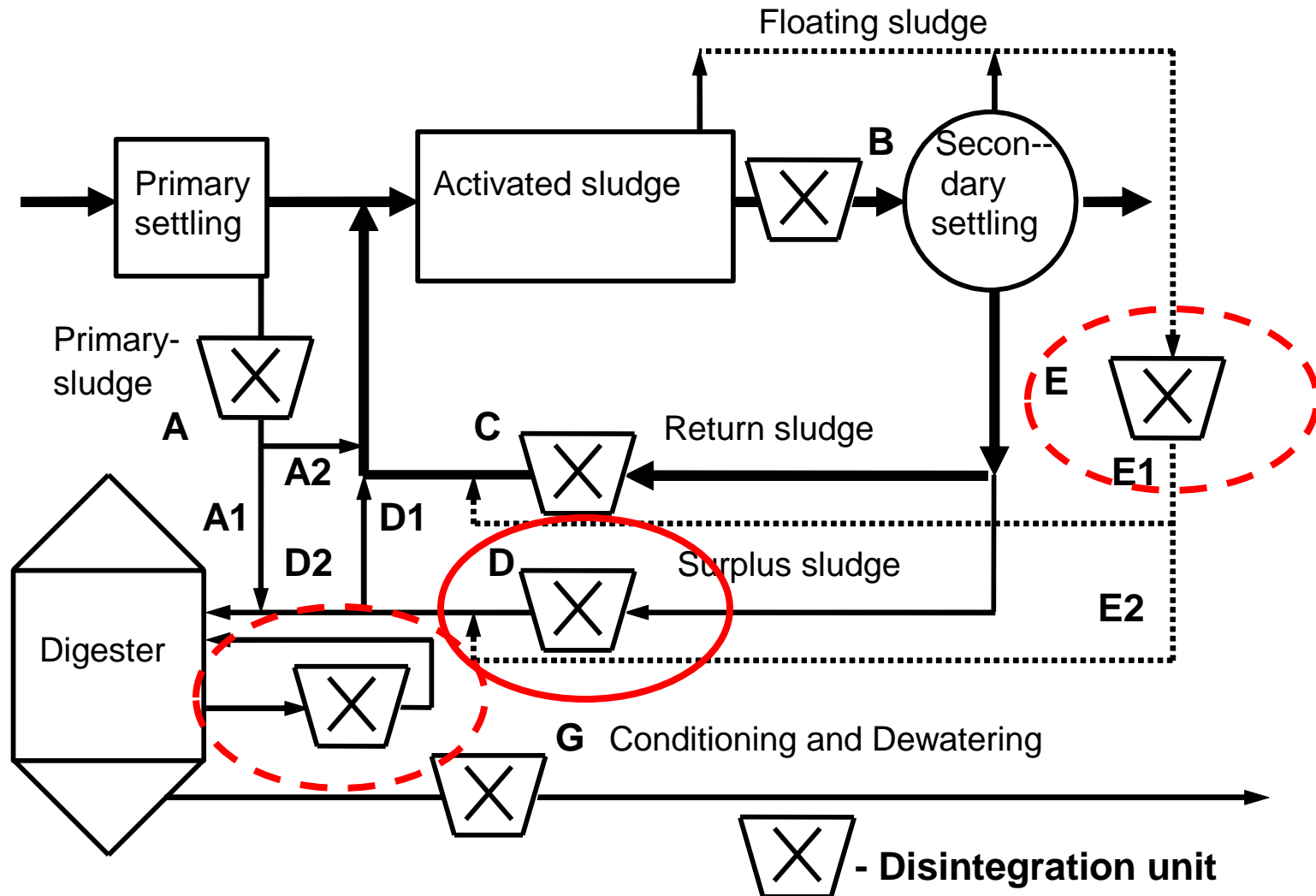






- Decrease in particle size
- Increase in soluble compounds (C, N, P)

# Locations for disintegration



- **Optimisation of digesting process**
  - Increase of biogas production
  - Reduction of sludge amount
  - Improvement of dewatering behaviour
- **Prevention / Reduction of operating problems**
  - Reduction of bulking sludge and foam
  - Improvement of settling characteristics
  - Prevention of cloggings
  - Reduction of sludge viscosity

## Secondary effects (selection)

- Increased return load of WWTP (COD, N, P, particles)
- Reduction of particle size (higher demand of polymers or change of polymers)
- Formation of organic compounds with low bioavailability
- Increase of pollutant-concentrations (e.g. heavy metals)
- Odour

- **Mechanical disintegration**

ultrasonic, mills, high pressure homogenisers, lysat centrifuge and other

- **Heat treatment**

temperature range from 80 to 180 °C, heat exchangers or direct steam

- **Oxidation processes**

partial oxidation using ozone and hydrogen peroxide

- **Biological treatment**

Autolytic processes, enzyme dosage, special micro-organisms, detergents, micronutrients

Methods available for full scale operation

- **Chemical treatment**

using acids or alkali, pH values below 2 or over 12

- **Freeze/thaw-treatment**

natural or technical freezing

- **Combinations**

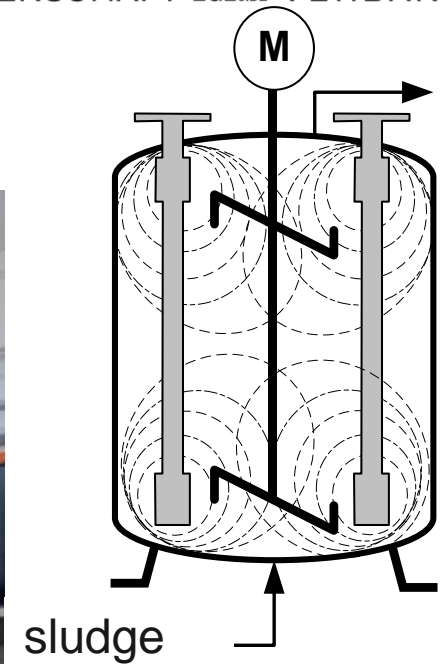
Heat/chemical, Mechanical/biological and other

- Generation of acoustic waves with high frequency ( $> 20$  kHz)
- Compression and expansion of the medium
- Cavitation and collapse of steam bubbles
- Destruction of flocs and cells through shear forces



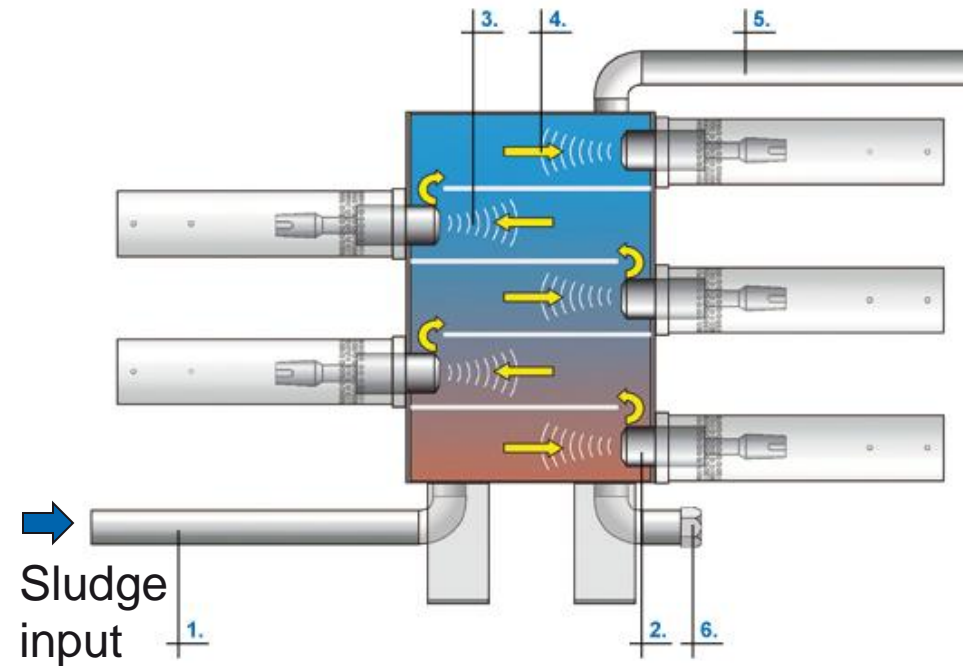
# Ultrasonic Disintegration

## Example: VTA



# Ultrasonic Disintegration

## Example: Ultrawaves/Sonotronic



- Input of heat (< 100 °C normal pressure, > 100 °C high pressure)
- Use of heat exchangers or steam injection
- Chemical and physical reactions
- Changes in cell-structure
- Break up of bio-chemical structures
- From 170 °C up increase of hardly biodegradable compounds (Maillard-reaction)

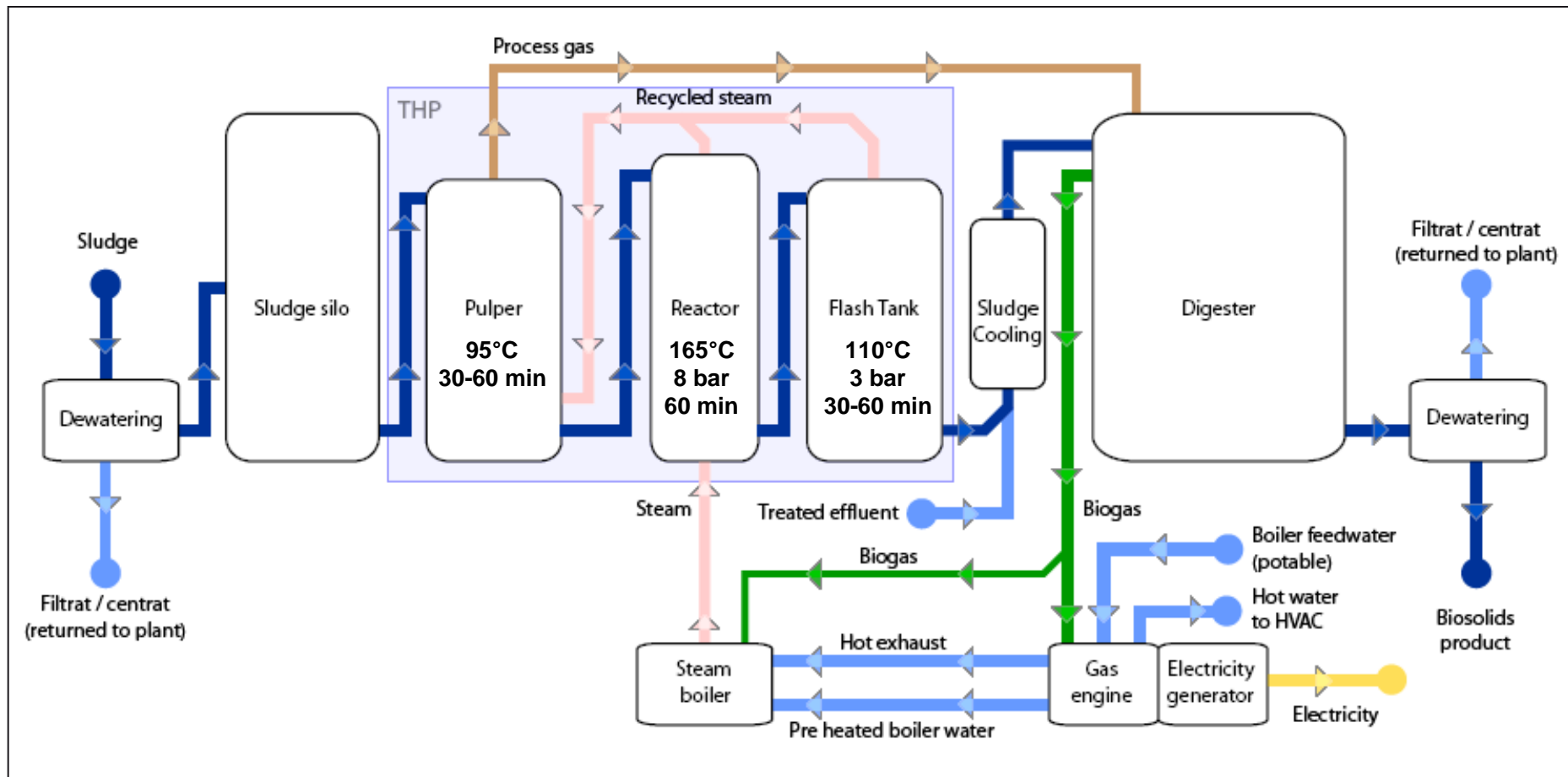
# Thermal hydrolysis

- **Provider:** Cambi, Veolia, (Stulz), Haarslev ...
- Working temperature 150 – 170 °C
- Input of heat: generally by steam injection



# Thermal hydrolysis

## Example: CAMBI



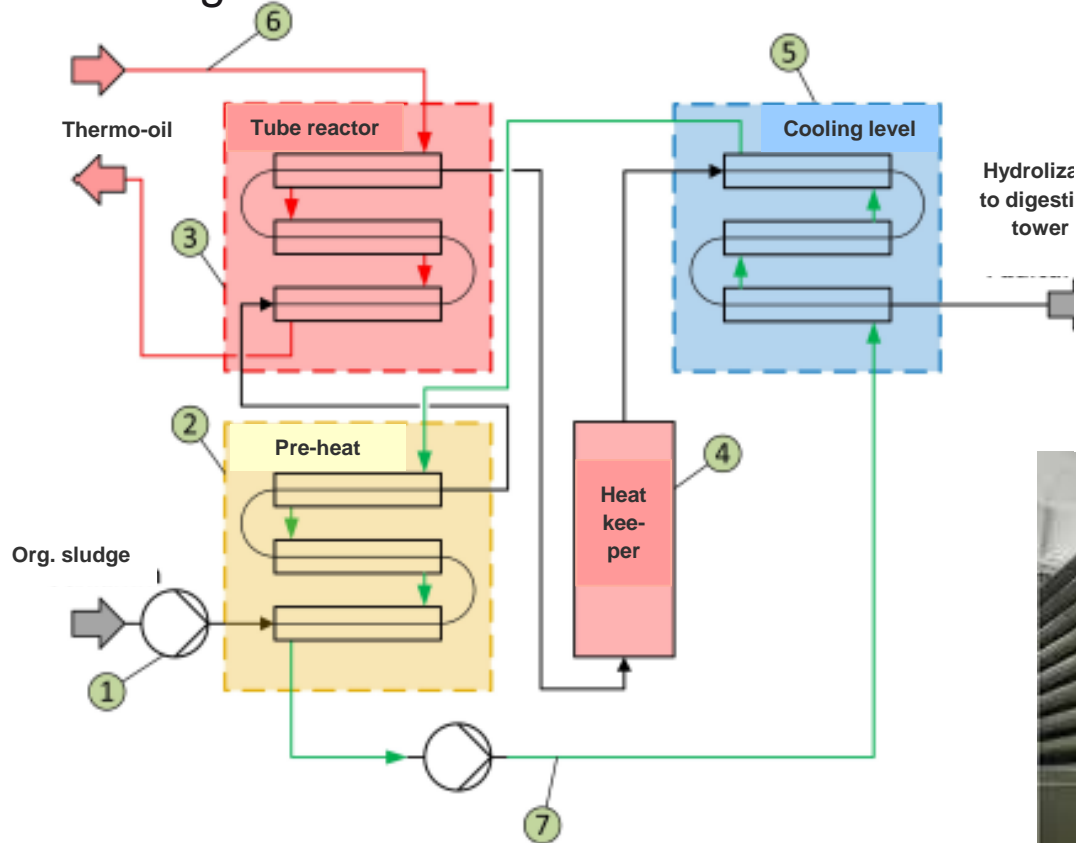
1 plant was operated in Germany (Geiselbullach)



# Thermal disintegration

## Example: Stulz (Lysotherm)

Heating with thermo-oil

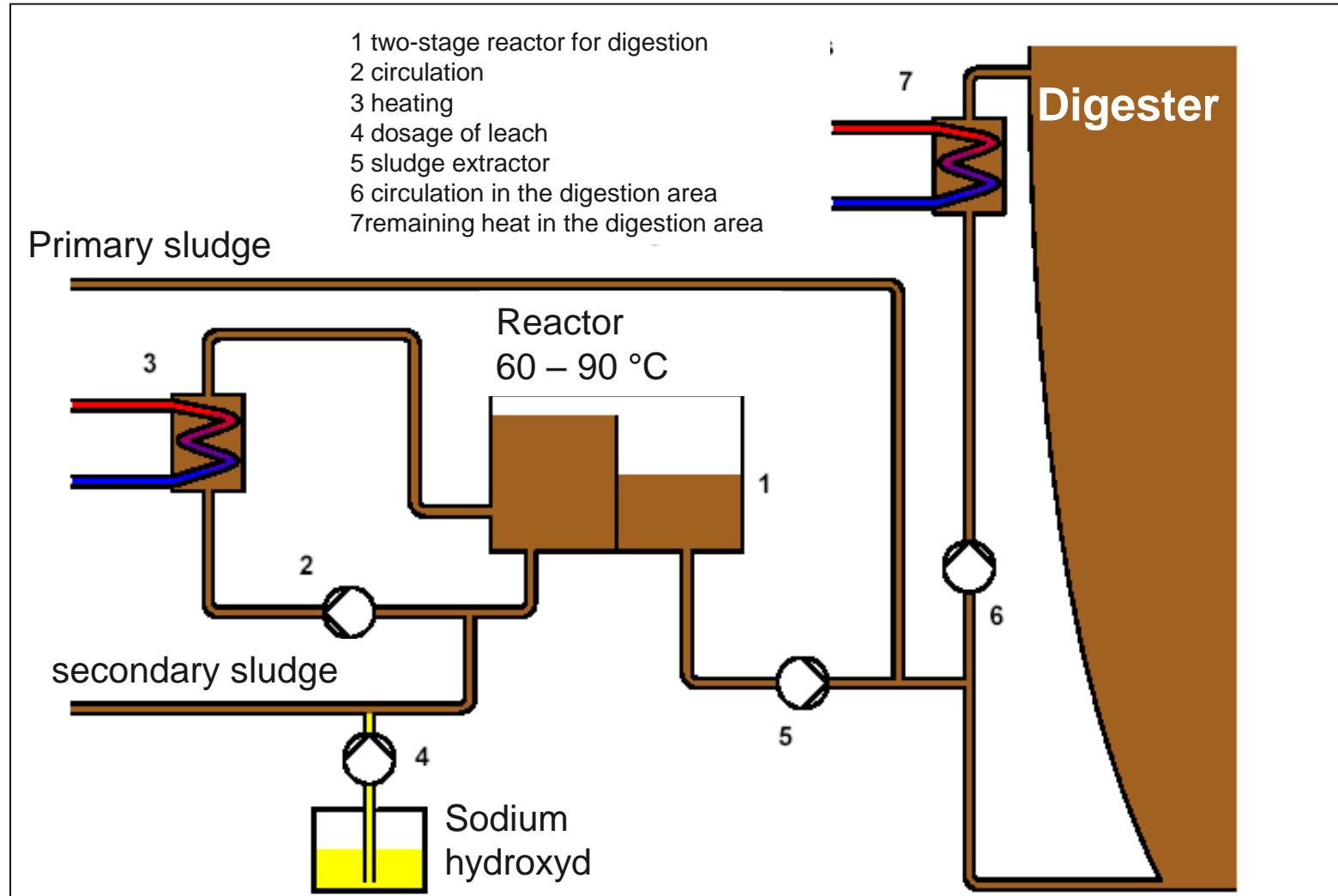


1 operating plant in Germany (Lingen)



# Chemical-thermal disintegration

## Example: Pondus



# Chemical-thermal disintegration

## Example: Pondus

- Treatment-temperature between 60 and 90 °C
- Additional dosage of sodium hydroxyd (ca. 2 l/m<sup>3</sup>)
- Use of exeed heat of the CHPP by heat exchanger
- Several operating facilities in Germany (Gifhorn, Ratekau, Uelzen)
- Capacity 700 - 1 000 t DS/a surplus sludge



- Catalysing the degradation
- Enzymes are specific for substrate and effect
  - „key - lock – principle“
- Speeding up the degradation of long-chained compounds
- Start up-dosage at the beginning (inoculation)
- Further dosage dependent on the sludge amount

- **Ultrasonic**

- Simple to integrate, low investment
- Limited effects (more biogas, low effect on dewatering result, effects direct dependent on energy input)
- Reasonable e.g. for poor working digesters

- **Thermal Disintegration**

- Medium investment for thermal-chemical disintegration (→ medium sized WWTPs)
- High investment for thermal hydrolysis (→ big WWTPs)
- Significant increase of gas production and degradation
- Improvement of dewaterability

- **Enzymes**

- Mainly product-costs, very low investment
- Limited effects (more biogas, improvement of clogging problems, very specific on the sludge)

# Results (overview)

	Method	Results	Remarks
mechanical	mechanical 0,5 KWh/m <sup>3</sup> – 20 KWh/m <sup>3</sup>	A <sub>CSB</sub> up to 20 %; η <sub>oTM</sub> up to 50 % higher; sometimes better settling behaviour and reduced foam	<ul style="list-style-type: none"> <li>• Need of electric energy;</li> <li>• Chemical composition is not changing if temperature is constant;</li> <li>• Ultrasonic is used on several WWTPs</li> </ul>
thermal	thermal 130 °C – 180 °C 130 kWh <sub>th</sub> /m <sup>3</sup> – 190 kWh <sub>th</sub> /m <sup>3</sup>	A <sub>CSB</sub> up to 50 %; η <sub>oTM</sub> up to 70 % higher; less foam, better dewatering results	<ul style="list-style-type: none"> <li>• Heat-energy cheaper than electric energy</li> <li>• Heat recovery up to 95 % possible</li> <li>• Formation of heavily degradable compounds</li> <li>• Desinfection of the sludge possible</li> <li>• several facilities for thermal treatment (160 – 180 °C) in Europe</li> </ul>
electro-magnetic	High-performance pulse technique, electro-kinetic disintegration		<ul style="list-style-type: none"> <li>• Only few investigations</li> <li>• Low operating costs, simple to integrate</li> <li>• Several operating facilities</li> </ul>

# Results (overview)

	Technique	Results	Remarks
chemical	Hydrolysis	with chemicals $A_{\text{COD}}$ up to 100 %;	<ul style="list-style-type: none"> <li>Neutralisation of the sludge with acids or bases, salting</li> <li>Particularity in the industrial WWT</li> </ul>
	Oxidation (Ozon) 0,05 g $\text{O}_3$ /g oDM– 0,2 g $\text{O}_3$ /g oDM 0,19 kWh/kg DS and 2,5 kWh/kg DS	Dependent on Ozondosage $A_{\text{COD}}$ up to 80 % $\eta_{\text{oDM}}$ up to 20 % higher	<ul style="list-style-type: none"> <li>Positive effects with very low ozon-dosages</li> <li>no current investigations for anaerobic digestion</li> </ul>
biologic	Hydrolysis	$\eta_{\text{oDM}}$ up to 30 % higher	<ul style="list-style-type: none"> <li>Low investment, easy handling</li> <li>On some WWTPs in operation, positive effects on floating cover and cloggings possible</li> </ul>
combi-nations	Thermal-chemical 60 °C – 70 °C 40 – 50 kWh/m <sup>3</sup> NaOH: 1,5 bis 2,0 l/m <sup>3</sup>	$A_{\text{COD}}$ up to 50 %; less foam, better dewatering results	<ul style="list-style-type: none"> <li>Use of low temperature heat</li> <li>Several facilities in Germany</li> </ul>



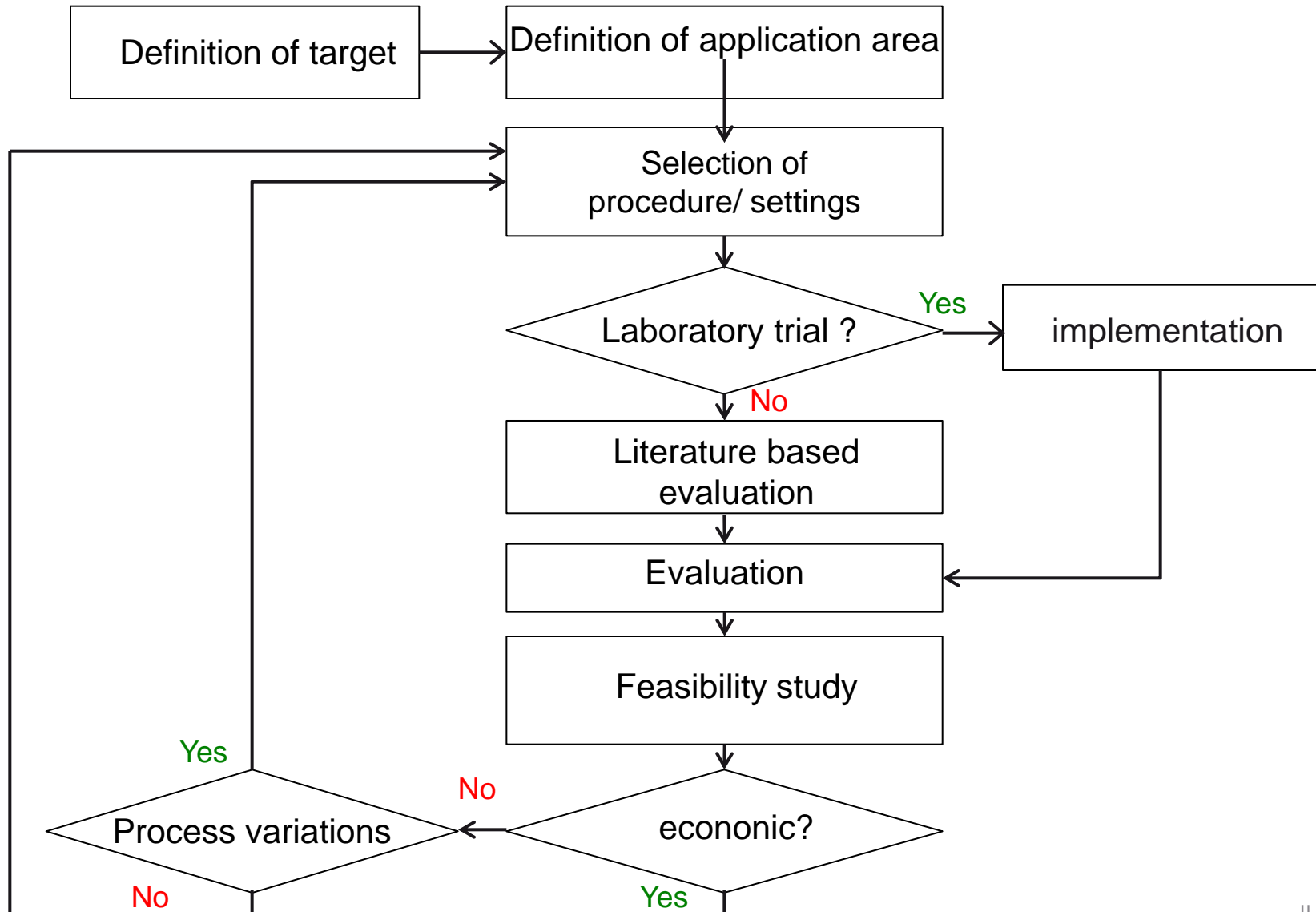
# Sewage Sludge Disintegration

## Selection of Techniques

Target for degree of disintegration $A_{\text{COD}}$	Generally required energy for disintegration	Suitable Methods
< 10 %	Low <10 kWh/m <sup>3</sup>	<ul style="list-style-type: none"> <li>• Electro-kinetic Disintegration</li> <li>• Hydrocavitation</li> <li>• Surfactants</li> <li>• Enzymes</li> <li>• Lysatcentrifuge</li> <li>• Ultrasonic</li> </ul>
10 % – 30 %	Medium >10 kWh/m <sup>3</sup> – < 50 kWh/m <sup>3</sup>	<ul style="list-style-type: none"> <li>• Ultrasonic</li> <li>• High-pressure homogenisers</li> </ul>
30 % – 50 %	High > 50 kWh/m <sup>3</sup>	<ul style="list-style-type: none"> <li>• Thermal methods</li> <li>• Oxidation (Ozon, H<sub>2</sub>O<sub>2</sub>)</li> <li>• Thermal-chemical methods</li> </ul>

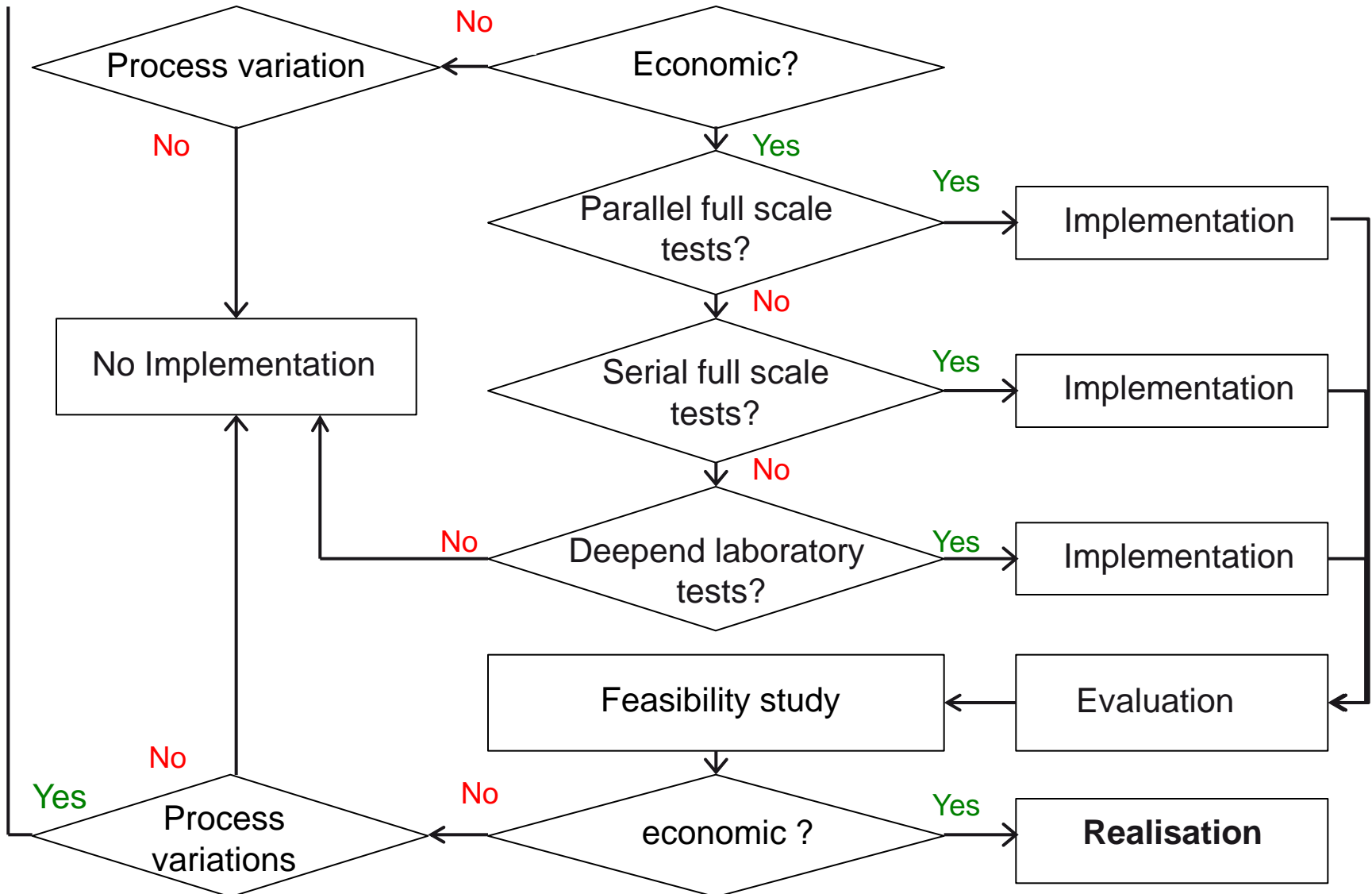
# Application of Sewage Sludge Desingetration

## Basic Procedure I



# Application of Sewage Sludge Desingetration

## Basic Procedure II



- **Application of Sewage Sludge Disintegration**
  - Preferred in secondary sludge
  - Optimisation of sludge characteristics (viscosity, settling, foam)
  - Release of organic carbon for better degradation especially in anaerobic digestion
  - Negative secondary effects are possible (N-reload)
  - In most cases a high energy input is needed for a drastic increase of degradation
- **Ultrasonic-, thermal disintegration and dosage of enzymes are successful for optimisation of anaerobic digestion on several WWTPs**
- **Installing of a disintegration technique requires previous tests**
- **Besides the energy balance, the primary and secondary effects must be considered for an economic application of disintegration on WWTPs**

**Thank you for your attention!**

