





### Variation of loading of WWTP - seasonal influences

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#### The coast line of Germany





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## Wastewater disposal in regions of tourism

#### **Special qualities**



- Seasonal changes
- Sudden peaks within a few days (very problematic)
- Strict effluent demands (discharge into bathing water)
- Increased amount of chemical toilets and fatty substances
- Often low alcalinity
  - Especially when using water supply out of dunes
- Design and operation of the sewage network and WTP
  - Problems with sediments, odour and corrosion in the sewers
  - Choice of wastewater treatment process
  - Case study of loading and dimensioning (e.g. dynamical simulation)





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#### **Comparison of daily fluctuations**





#### Typical variation of the daily inflow

Seaside resort (Westerland/Sylt)





#### Changes of the wastewater content



- Increase of the concentrations during season
  - ➡ Organic Matters (BOD<sub>5</sub> u. COD)
  - $\Rightarrow$  Nitrogen (KN or NH<sub>4</sub>-N)
  - Phosphorus
  - Suspended solids (SS)
  - Increase of fatty substances

from 10% to 40% from 20% to 100% up to 50% from 15% to 50%

- Sudden peaks (example New Years Eve ):
  - Doubling of the wastewater amount
  - → 2.5-times of the organic load
  - 3-times of the load of nitrogen

#### Wastewater discharge systems

Special requirements



- Gravity sewer system
  - $\rightarrow$  Dimensioning with  $Q_{h,max.}$
  - Increase of deposits (higher frequency of rinsing necessary)
  - Higher amount of infiltration water
- Pressure pipe systems
  - Dimensioning with maximum flow (m<sup>3</sup>/h) in the season
  - Pumps (Twin Pump station, frequency regulated pumps, etc.)
  - Parallel pipes with different nominal size
- Odour and corrosion problems
  - Flushing with pressured air
  - Biofilter for odour treatment
  - Dosage of agents with chemical or biological effect (e.g. FeCl<sub>3</sub>, NO<sub>3</sub>)



# Joint treatment - content of chemical toilets



#### • Origin

- Delivery directly to WTP
  - e.g. via camper vans, tanker or buses, cruiser ships)
- Discharge into the public sewer system (problem of control)
- Loads

Toxic substances

- About 40-times higher COD
- About 1,000-times higher nitrogen concentrations
- Important conditions for joint treatment
  - Determination of actual capacity of treatment plant
  - Least capacity of the WTP is 10,000 PE
  - Equalised dosage; regarding a 20-times dilution ratio

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- Determined by Alkaline hardness of potable water +Hydrolysis of KN
- Negative influence on nitrification
- Destruction of the floc structure leads to sludge discharge
  - Decrease of the sludge age and loss of nitrification
- ✤ Decrease of the pH-value
  - Inhibition of the nitrifyers

Solutions:

- Dosage of alkaline precipitation agents
- Denitrification to highest degree

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## Alkalinity





#### **Denitrification to highest degree**







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#### Methods of wastewater treatment

- Several lines
- Chemical-treatment
  - Dosage of chemicals during season
    - Precipitation and flocculation agents
    - External carbon-sources
  - Separate line during season (no nitrogen removal)
- Activated sludge system
  - "Raising" of the content of dry solids (MLSS) up to the technically possible limit
  - Hybrid system suspended biomass plus moving bed
  - Regulated raw sewage storage tank
  - External storage tanks for nitrifyers
  - Hybrid method ("two-stage" in time of peak load, one-stage during normal operation)

#### Combination of activated sludge and biofilter

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#### Dimensioning the activated sludge system



#### Case studies of loading is necessary!

- ➡ Maximum BOD<sub>5</sub> load
  - High surplus sludge production, unfavourable for nitrification
- ➡ Worst BOD<sub>5</sub>/N ratio
  - Unfavourable for denitrification
- Average load during the season
- Considering of peak loads
  - Low temperature and crucial holidays
- Tools for design and calculation
  - Stationary Methods
    - problem: short term fluctuations can not be recorded
  - Dynamic simulation, e.g. according to ASM1 or ASM 2 of IWA

#### Semi-technical investigations



# Dimensioning using dynamic simulation calculation



- Measuring series to record
  - Peak loads
  - $\Rightarrow$  wastewater parameter (e.g.: 2-h-samples COD; KN, NH<sub>4</sub>, NO<sub>3</sub>, tot.P.)
- Determination of biological parameters from the pilot plant (µ, yield, inhibition effects etc.)
- Building up a model of the existing plant



- Verification of the model
- Modelling various new designed treatment plant concepts
- Proof of the efficiency for different case studies

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#### **Results of dynamic simulation Example WWTP Westerland**



Load case: "Thunder strom" Summer max.N<sub>anorganic</sub> = 6 mg/l Load case Christams/New years eve max.N<sub>anorganic</sub> = 7,6 mg/l



#### Limiting value N<sub>anorg.</sub> 10 mg/l

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#### Technische Final design of the WTP Westerland/Sylt Universität





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#### **Example KA Lütjenbrode Expansion for final Denitrification**





- Capacity 50.000/85.000 PE
- Inlet
  - Screen/gritchamber
- Large primary settler
  - V 1.320 m<sup>3</sup>
- 2 Tricking filter
  - 4.660 m<sup>3</sup> BioNet
- Activated stage
  - V<sub>BB</sub> 1.060 m<sup>3</sup>
- Sandfilter
  - A 120 m<sup>2</sup>; H 2 m

#### Combination activated sludge/fixed bed reactor

**Example WTP Heiligenhafen/Baltic sea** 



Load: Winter: 50,000 PE Summer: 85,000 PE

Plant design:



#### **DynaSand-Deni** Example: Final denitrification in summer



#### **Dosage of carbon source**





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#### DynaSand-Deni Operation results: summer time







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### **Example WTTP Zingst**



- Average Load ca. 9.200 PE; peak load: upto 14.000 PE
- Basic treatment performance
  - → very good COD,  $BOD_5$  efficiency (> 90%)
  - N-elimination liegt mit über 70%
  - Drift of suspended solids in the season
  - High loads appear in a short period (ca. 2 month)
- Challenges
  - Unclear capacity of the WTTP
    - -No expansion of settlement allowed by water authority
    - -No future development of tourism
    - -Summer house park connection was forbidden
  - No sufficient oxygen supply in the season
  - Bulking sludge ; drift of sludge





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#### WTTP Zingst **Year of 1999**



#### Daily wastewater flow over the year







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#### Curve of daily flow (high season) Example WTP Zingst/Darss





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#### Modell of the activated sludge system





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#### Time

#### **Results and recommendations**



- The rotation disc plant should be only used as a buffer
  - Enlargement of the capacity by 1.600 PE
- Existing seasonal load can be covered by improved aeration system
- Buffer and improved aeration covers a load of 11.000 PE
- Short term load increase of 1.800 E can be provided
  - No limitation of short term touristic development
- For future loads the plants has to be rehabilitated



#### WTTP Zingst Today







## Determination of the treatment capacity WTTP Körkwitz using dynamic simulation

#### Introduction



 Capacity of the WTTP Körkwitz according water law permission from 1987 was 187.000 PE

COD was limited to 200 mg/l; BOD<sub>5</sub> to 130 mg/l

➡ In future COD: 90 mg/l, N: 18 mg/l, P: 2 mg/l

- Changed conditions through the collapse of the main industry (fibreboard factory (IKEA))
  - No exact classification for the size of the WTTP to the objectives of treatment was possible
  - Water authorities had forbidden to build up new residential sites of hotels without a proof of capacity
  - Investigation of the actual capacity of the WTTP was necessary
  - Tool: measurement campaign and dynamic simulation

# Determination of the input data for the simulation Measurement programme (July)



#### **Objective**:

Determination of the inlet and outlet parameters Sketch of the plant



Location of samples during the measure campaign

#### Determination of the input data for the model



Concentration graph (2-h) in the inlet of the activated tank Berlin





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## Execution of the simulation

Model of the WTTP Körkwitz made with SIMBA® Universität Berlin





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#### **Execution of the simulation**

**Results of the calibration (NH<sub>4</sub>-N-out)** 





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#### **Execution of the simulation**

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#### **Results of the calibration (NO<sub>3</sub>-N-out)**



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### **Procedure of the simulation**

#### **Case studies**



- Objectives of the simulation studies:
  - Determination of the capacity limitation of the WTTP Körkwitz with different loading situations
- Increasing the inlet load step by step (5.000 PE) starting on the load of the measurement period (42.200 PE)
- Case of loading, which have been considered:
  - ➡ 42.200 PE, 15°C
  - ➡ .....
  - ➡ 52.000 PE, 15°C
  - ➡ 41.500 PE, 10°C
  - ➡ 55.000 PE 15°C; buffering tank in the inlet



#### Summary



- Changes in amount and quality
  - Seasonal fluctuation
  - Sudden peaks
- Dimensioning of the treatment plants
  - Case study of loadings
  - Dimensioning of plant with dynamical simulation and additional pilot-plat investigations
  - Adapted treatment technology ("breathing" plant)
- Other specialities
  - Sewer system (sediments, max. flow, odour and corrosion)
  - Wastewater disinfection (UV- Irradiation)
  - Chemical toilets





## **Objectives for modelling a WTTP**



- Optimized design of the plant
  - Minimising the tank volume
  - Comparison of different variations of process technologies
  - Creating and adapting the control strategy
  - Combination with existing technologies
  - Design of mechanical and electrical equipment
- Estimations of future loading scenarios
  - Connection of new industries
  - New residual areas
  - Variation of load scenarios
- Determination of the capacity of exiting WTTP
- Optimizing the operating of the plant
  - Energy optimisation
  - Effect on the operation performance
  - Integrated Simulation
  - Education of the operation personal



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