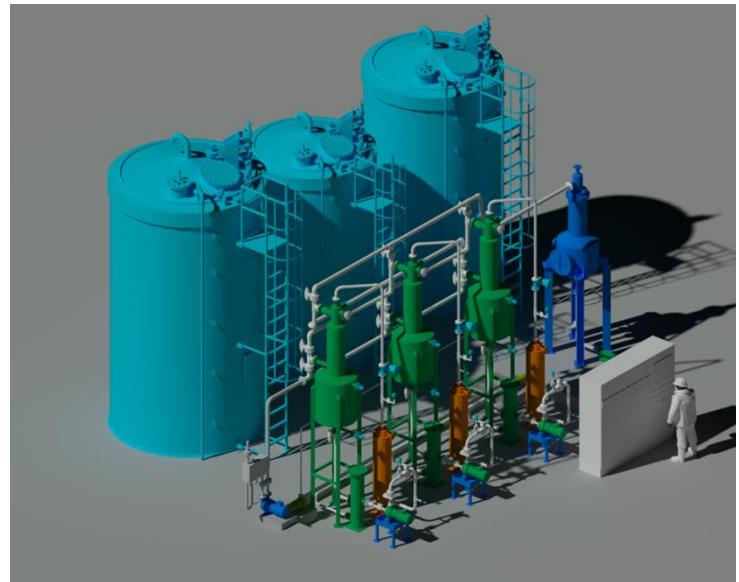


# Activating of the digester with thermal chemical hydrolysis and recovery of nitrogen

Thermal-Chemical Hydrolysis process  
(TCHP)



PONDUS-N: Recovery of nitrogen

# Nutrient reduction and recovery, Kalmar 2018



Thermal-chemical Hydrolysis



Degassing for digested  
sludge



Drying plants



Pasteurization



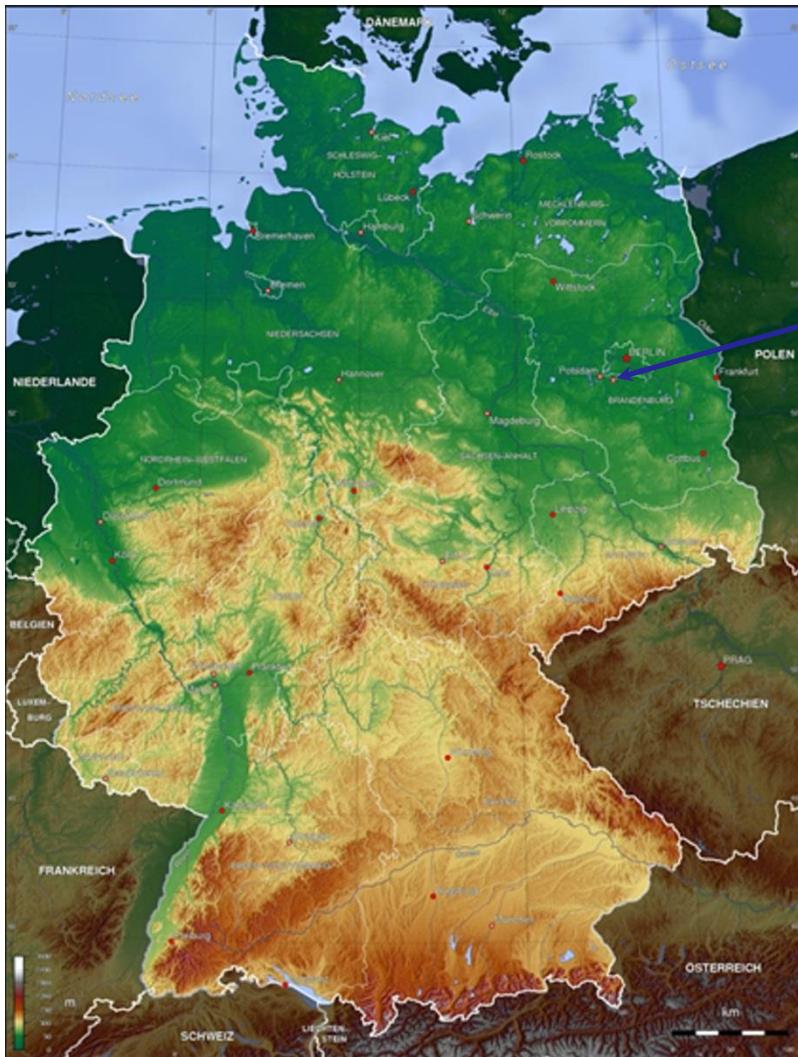
Mechanical defoamers



Substrate receiving and processing

**Different plants/systems of the company PONDUS**

# Nutrient reduction and recovery, Kalmar 2018



PONDUS Verfahrenstechnik GmbH  
near the capital Berlin  
in Teltow



Mr. Dr.-Ing. Andreas Dünnebeil

Where we are

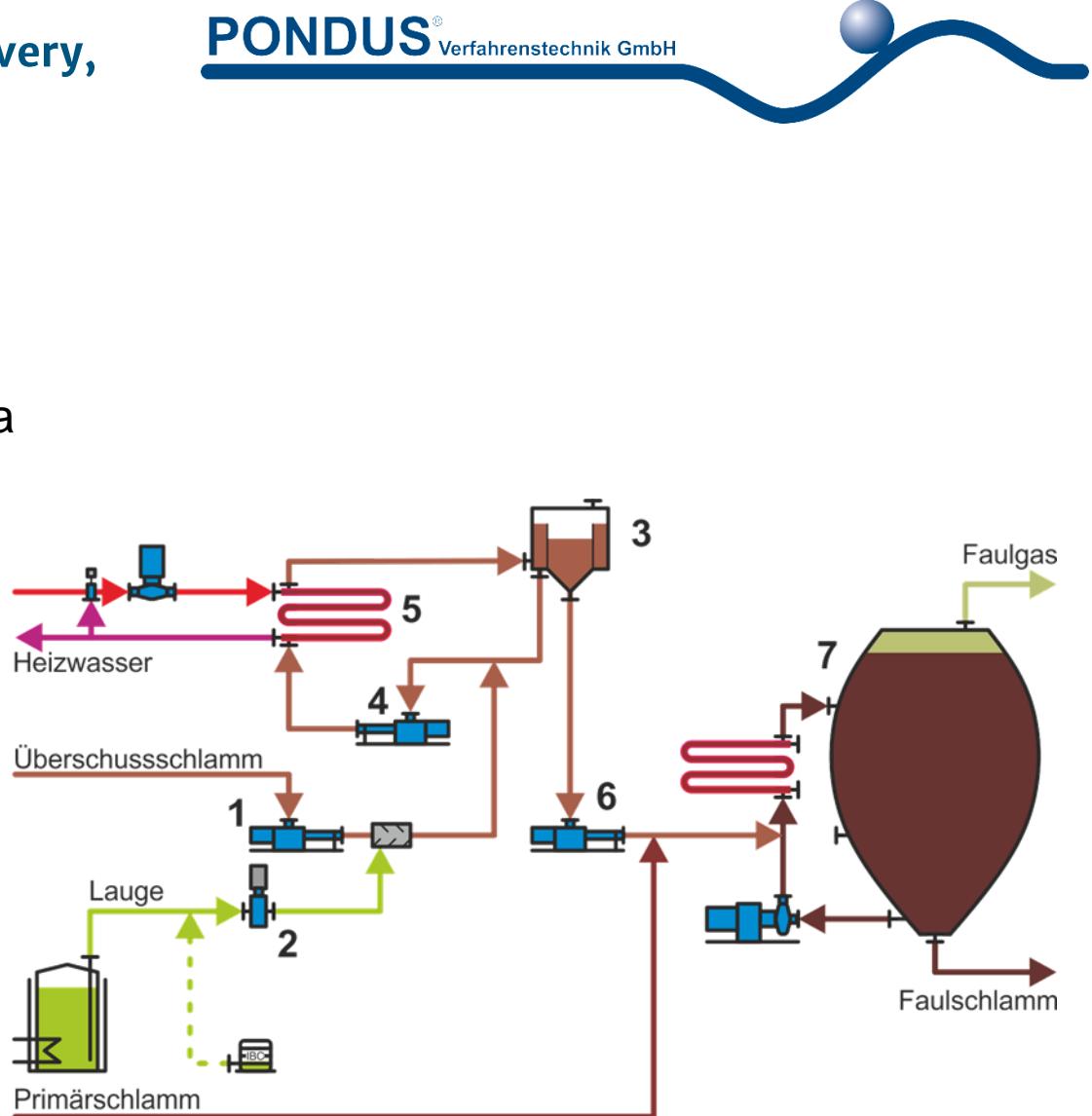
## Why we hydrolyse sludge ?

-  The gas production of activated sludge in comparison to the primary sludge is very low
-  We separate the process of hydrolysis out of the digester
-  We relieve the overloaded digester
-  We reduce the sludge production
-  We boost the gas production

Process for thermal-chemical hydrolysis

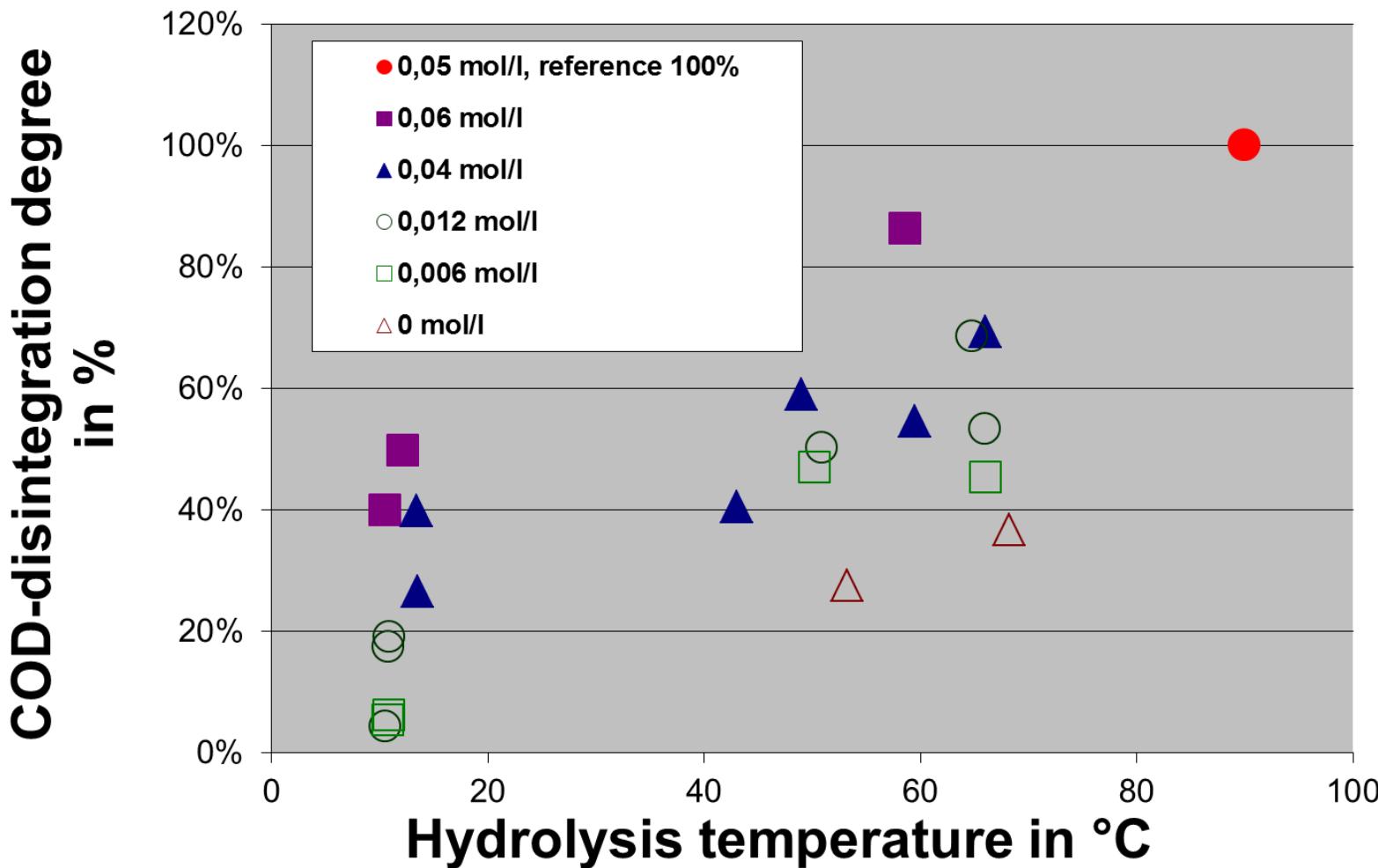
Why

- 1 Feed pump WAS
- 2 Dosing pump caustic soda
- 3 Reactor
- 4 Circulation pump
- 5 Heat exchanger
- 6 Discharge pump
- 7 Circulation digester

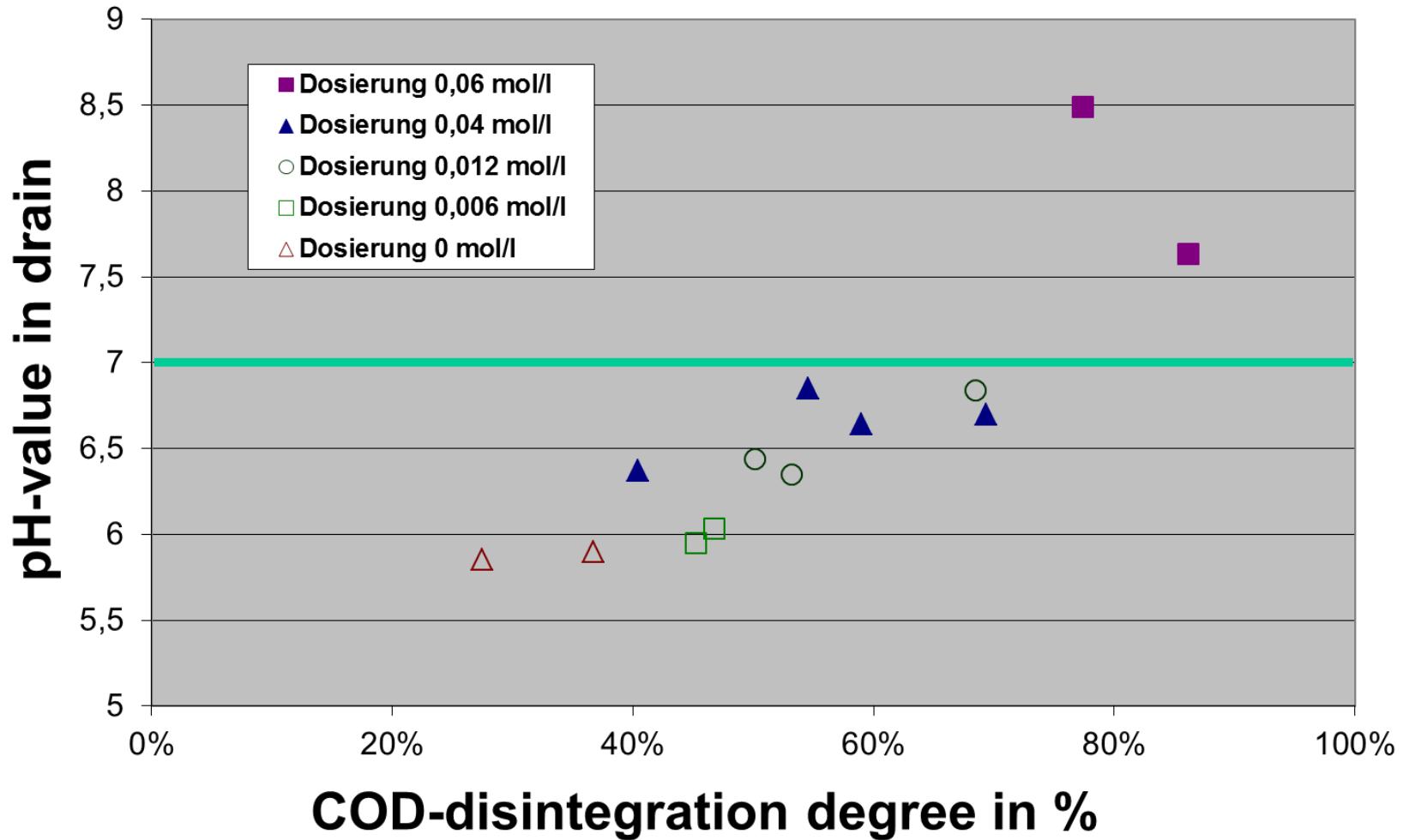


Process for thermal-chemical hydrolysis  
The process

## Nutrient reduction and recovery, Kalmar 2018



Process for thermal-chemical hydrolysis  
COD disintegration degree,  $f(T, \text{NaOH})$



Process for thermal-chemical hydrolysis  
pH-Level in drain

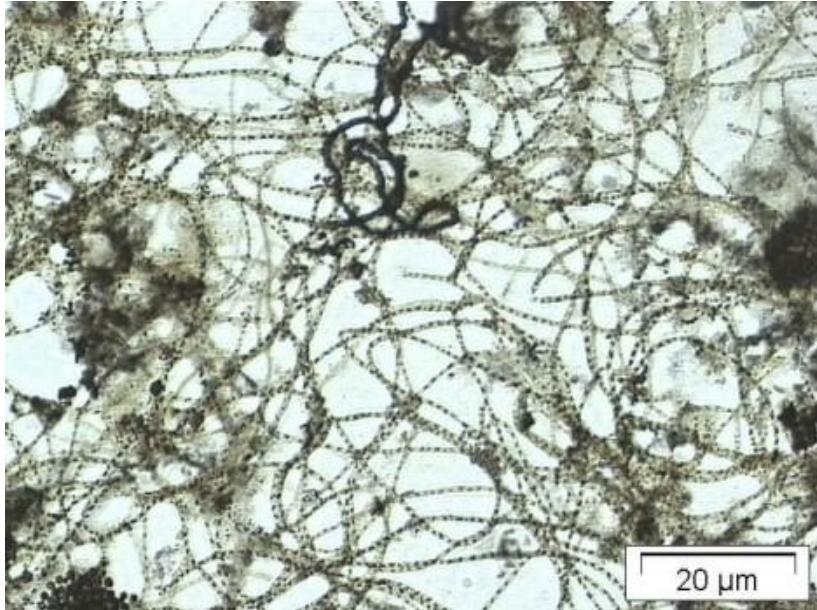


**Untreated waste activated  
sludge before hydrolysis**



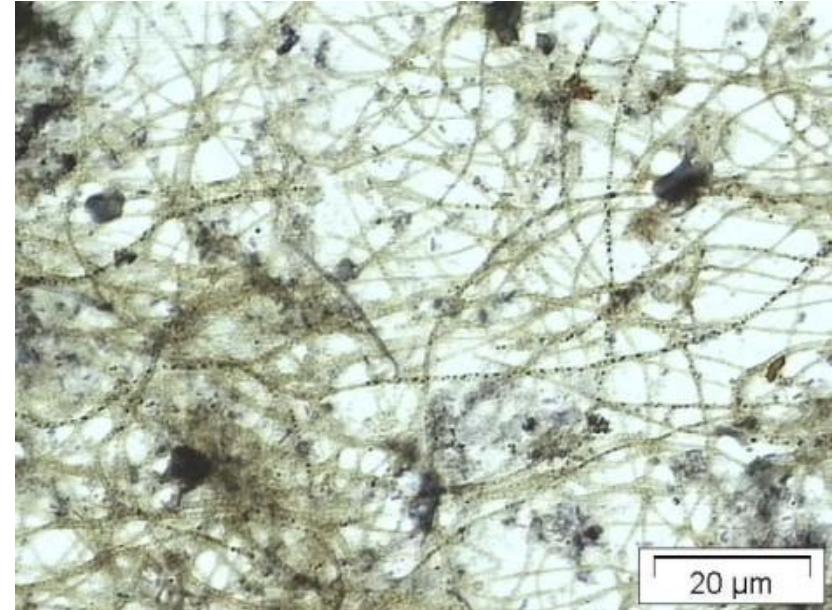
**Treated sludge after thermal  
chemical hydrolysis**

**Process for thermal-chemical hydrolysis  
Destruction of flakes and cells**



**Untreated waste activated  
sludge before hydrolysis  
with phosphorus  
(black points)**

**Process for thermal-chemical hydrolysis  
Discharge of phosphorus with hydrolysis**



**Treated sludge after thermal  
chemical hydrolysis  
without phosphorus inside**

At  
Chemisch-thermische Desintegration von  
Schwimmschlamm, Bernd Heinzmann, Gerd  
Engel, KA 2007, Nr. 4

- Increase of biogas production between 20 to 35%
- Reduction of sludge quantity
- Savings in polymer consumption at least 10 – 20%
- Reduction of sludge viscosity by up to 80% leading to better mixing with less energy
- Reduction or elimination of digester foaming
- Atmospheric pressure system, heating source is hot water from CHP- no steam or hot oil required
- Low energy requirement, no additional heat necessary
- Flexible adaptation of the process to changing operating conditions
- Simple operation and low O&M costs

**Process for thermal-chemical hydrolysis  
Benefits of thermal-chemical Hydrolysis**

## Nutrient reduction and recovery, Kalmar 2018

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for 30 – 40 m<sup>3</sup>/h



for 2,2 m<sup>3</sup>/h

**Process for thermal-chemical hydrolysis  
Reactor for big and small systems**

## Nutrient reduction and recovery, Kalmar 2018



High performance  
pipe in pipe  
Heat exchanger 1900 kW



Spiral  
heat exchanger  
260 kW



Conventional pipe in pipe  
heat exchanger 135 kW

**Process for thermal-chemical hydrolysis  
Different kind of heat exchanger**

Nutrient reduction and recovery,  
Kalmar 2018

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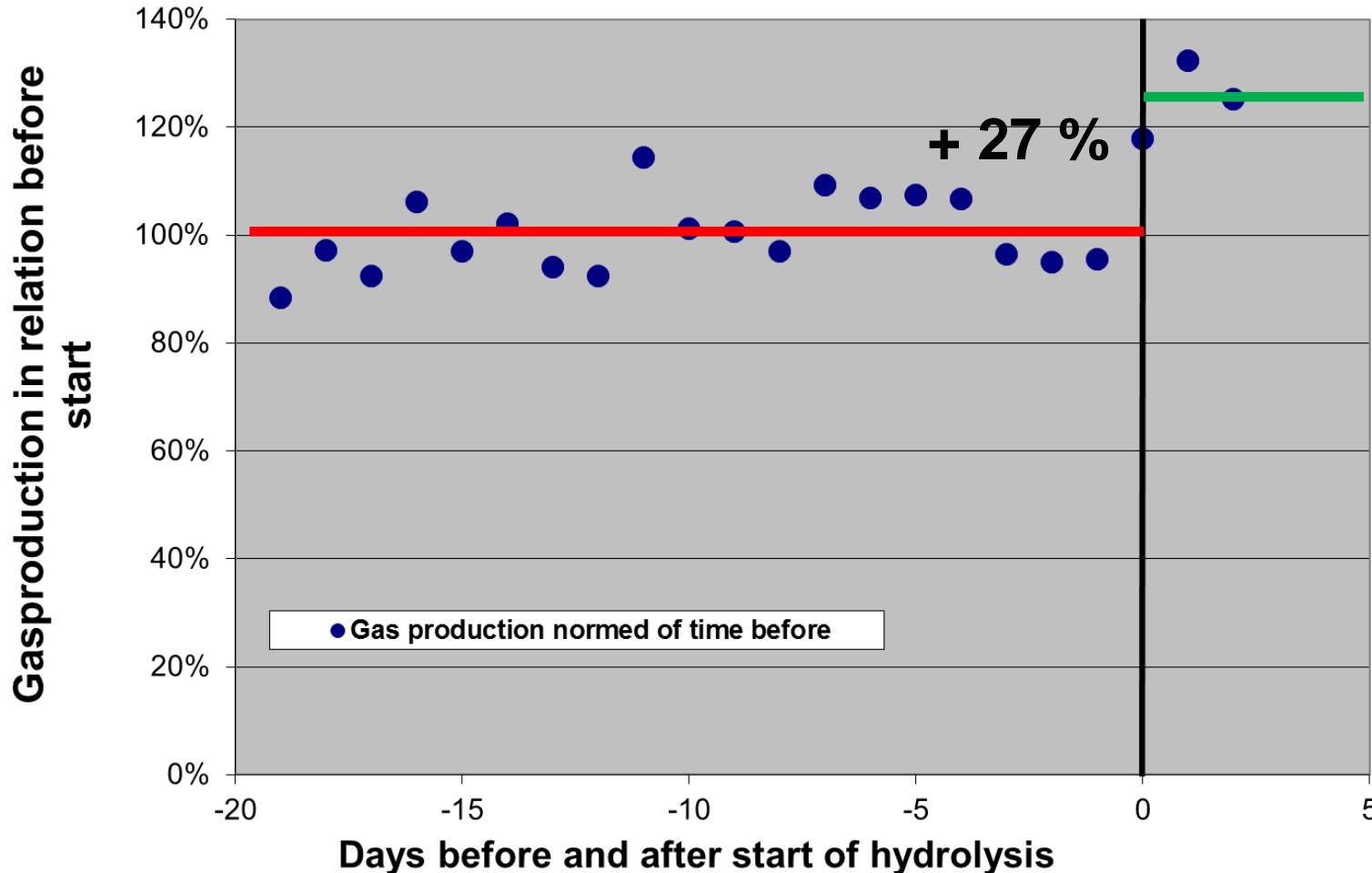
PE-Tank 20 m<sup>2</sup>

2 x IBC-Container

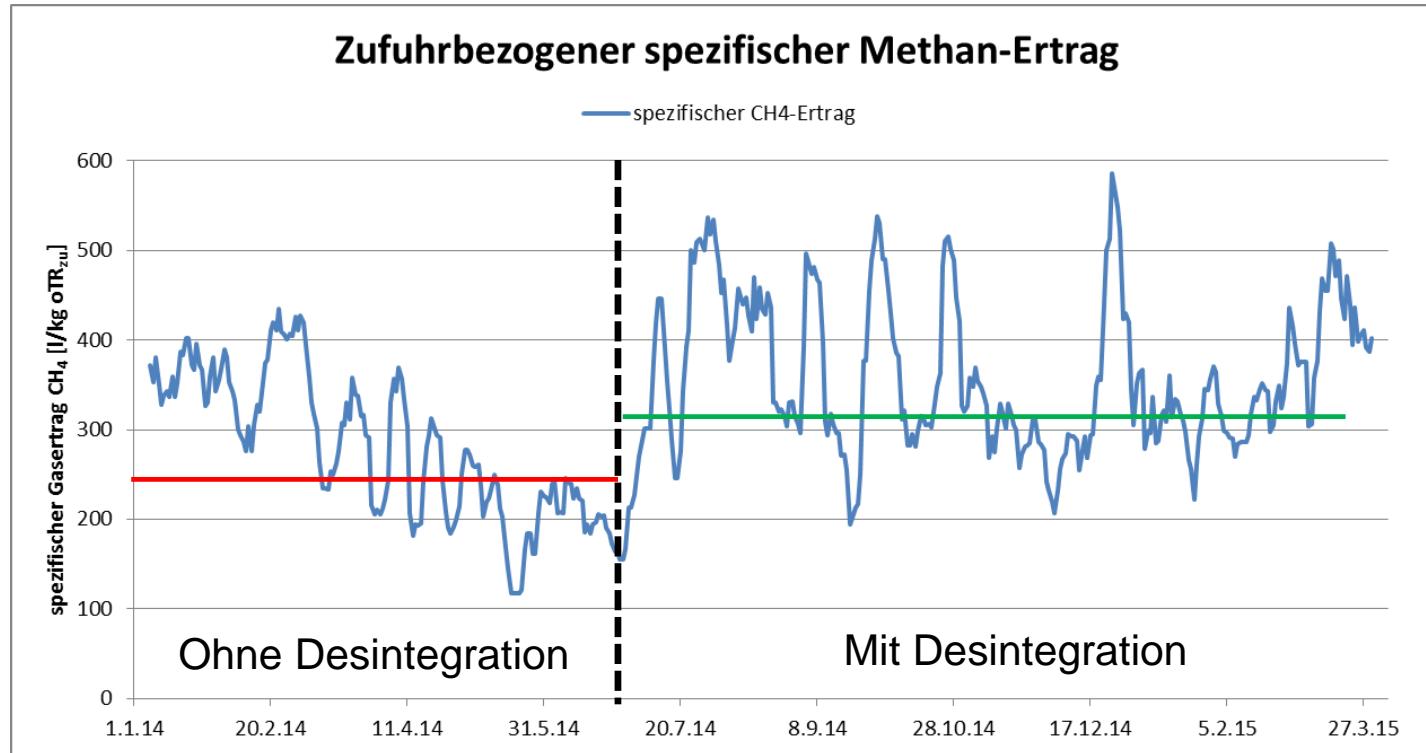


Process for thermal-chemical hydrolysis  
Storage of caustic soda

## Nutrient reduction and recovery, Kalmar 2018



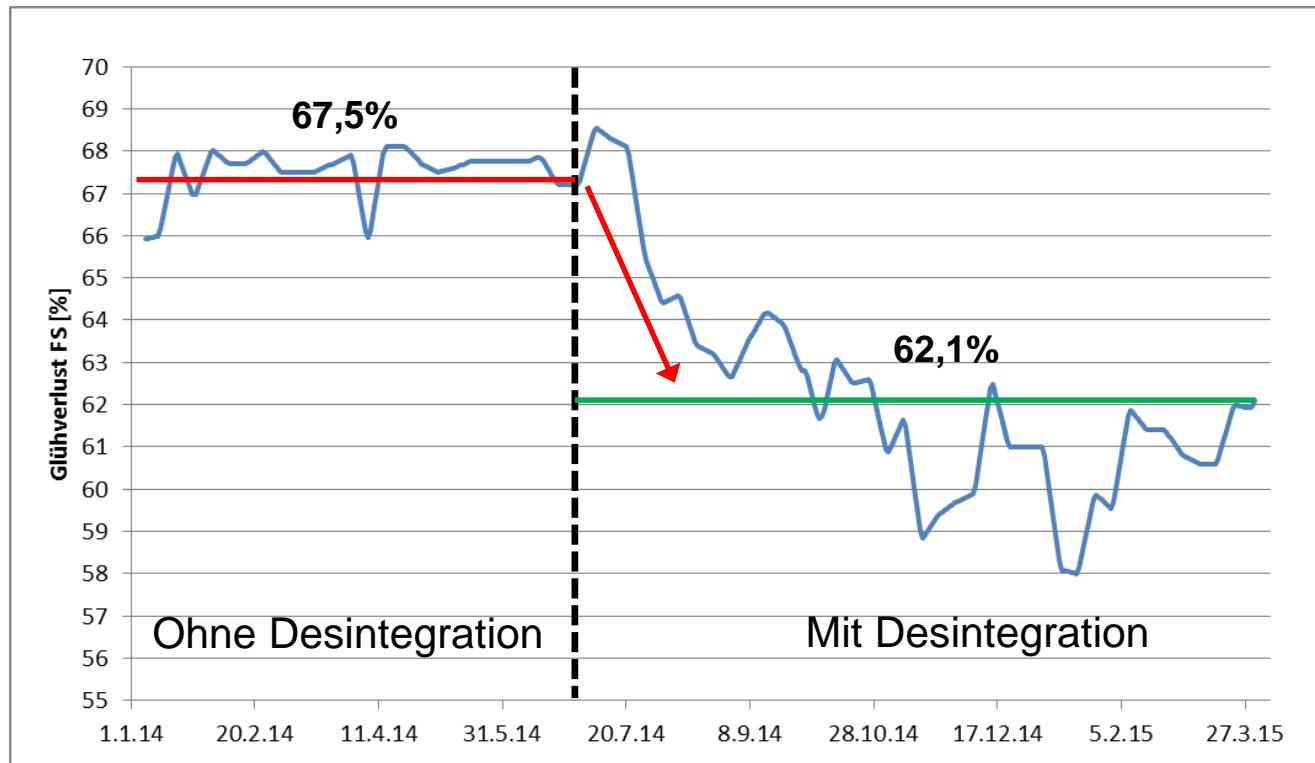
Process for thermal-chemical hydrolysis  
Increase of biogas production, Gifhorn



- ▶ Methanproduction without hydrolysis: i.m.  $239 \text{ l/kg oTR}_{\text{zu}}$
- ▶ Methanproduction with hydrolysis: i.m.  $312 \text{ l/kg oTR}_{\text{zu}}$  + 31 %

Process for thermal-chemical hydrolysis  
Increase of gas production, Uelzen

## Nutrient reduction and recovery, Kalmar 2018

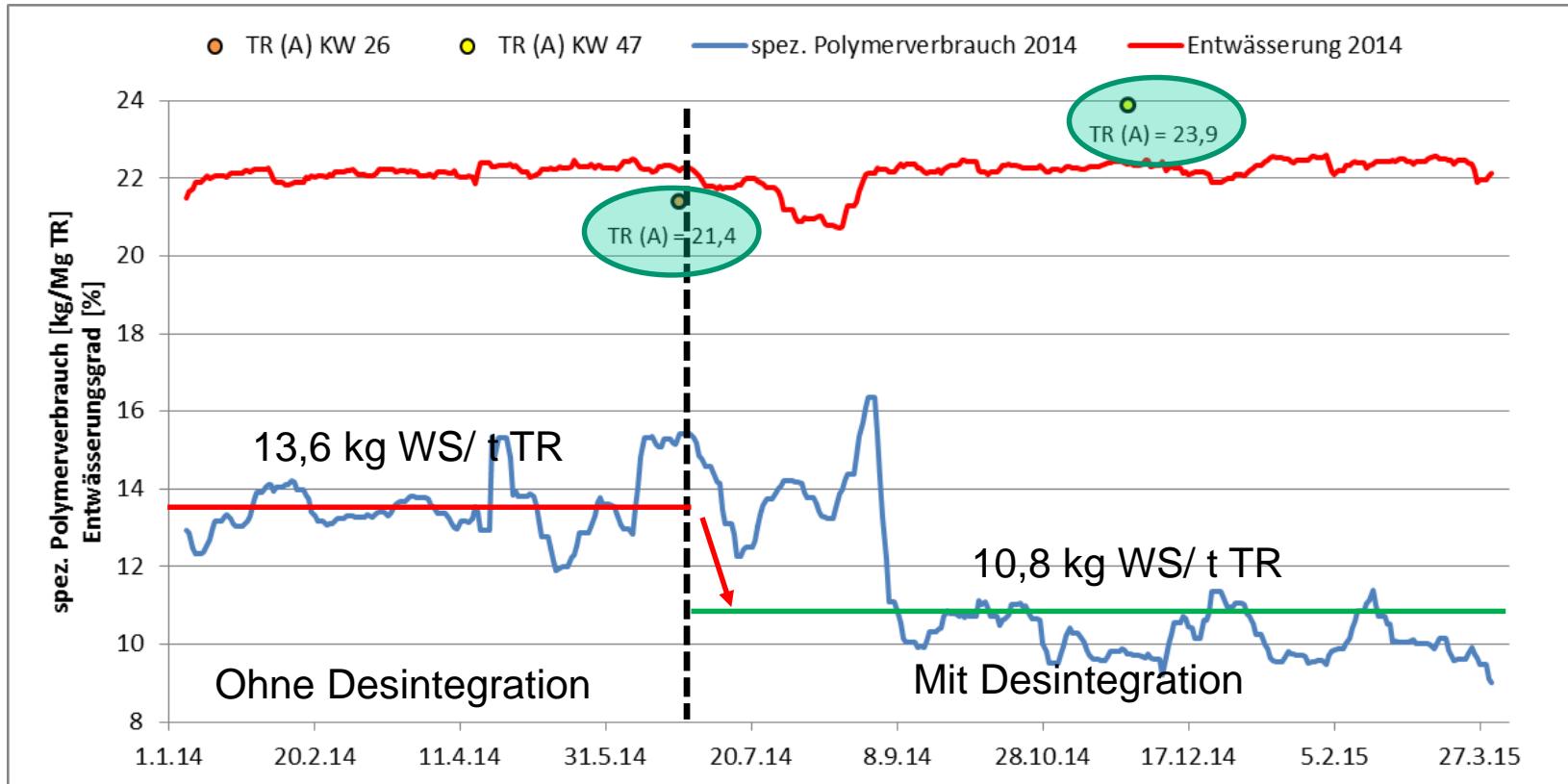


Glühverlust (berechnet) im Rohschlamm vergleichbar (ohne/mit Des.: 87,5/87,9%)

- ▶ Loss of lost ignition in digested sludge 5,4 %-point (-9% relativ)

**Process for thermal-chemical hydrolysis  
Loss of lost ignition in digester, Uelzen**

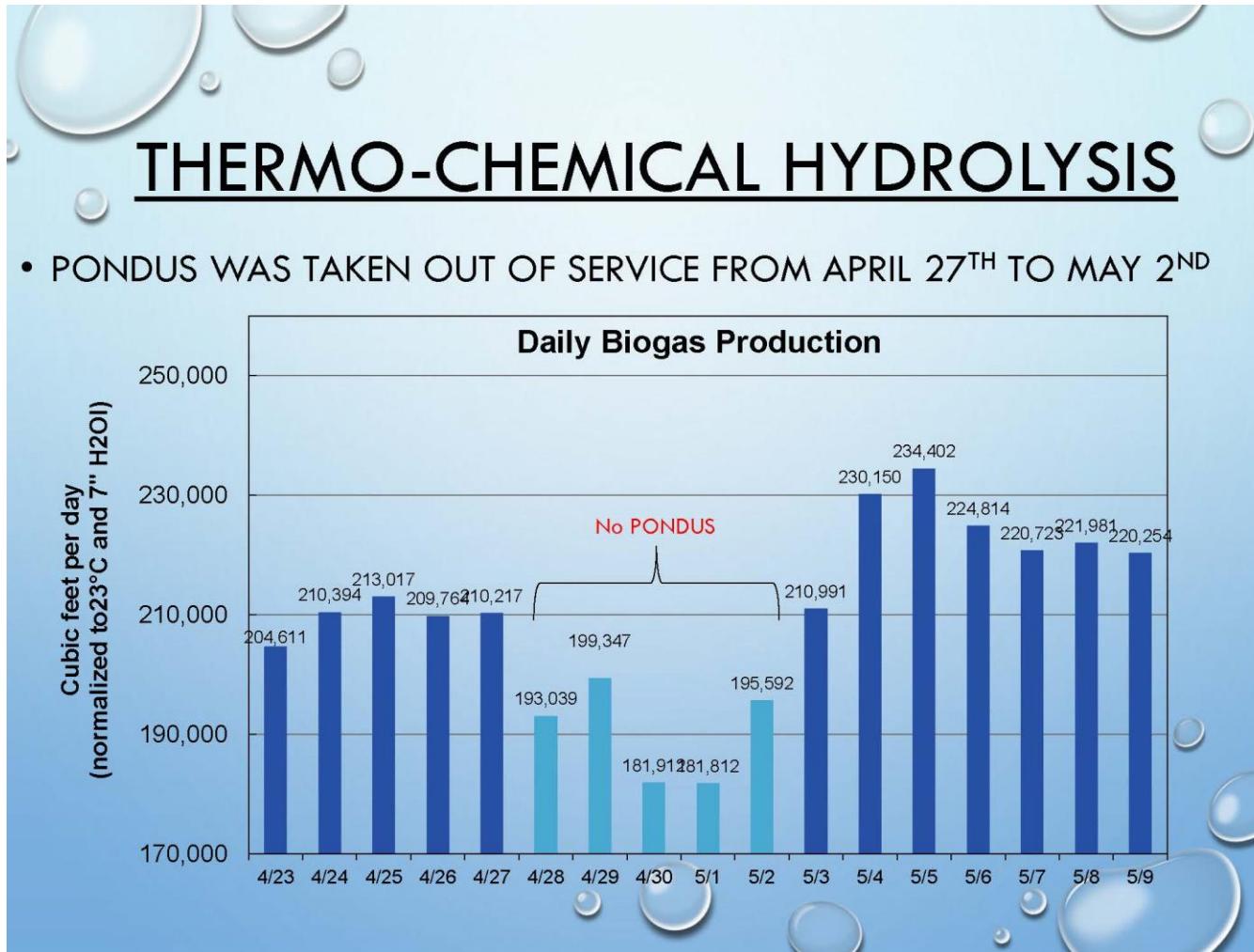
# Nutrient reduction and recovery, Kalmar 2018



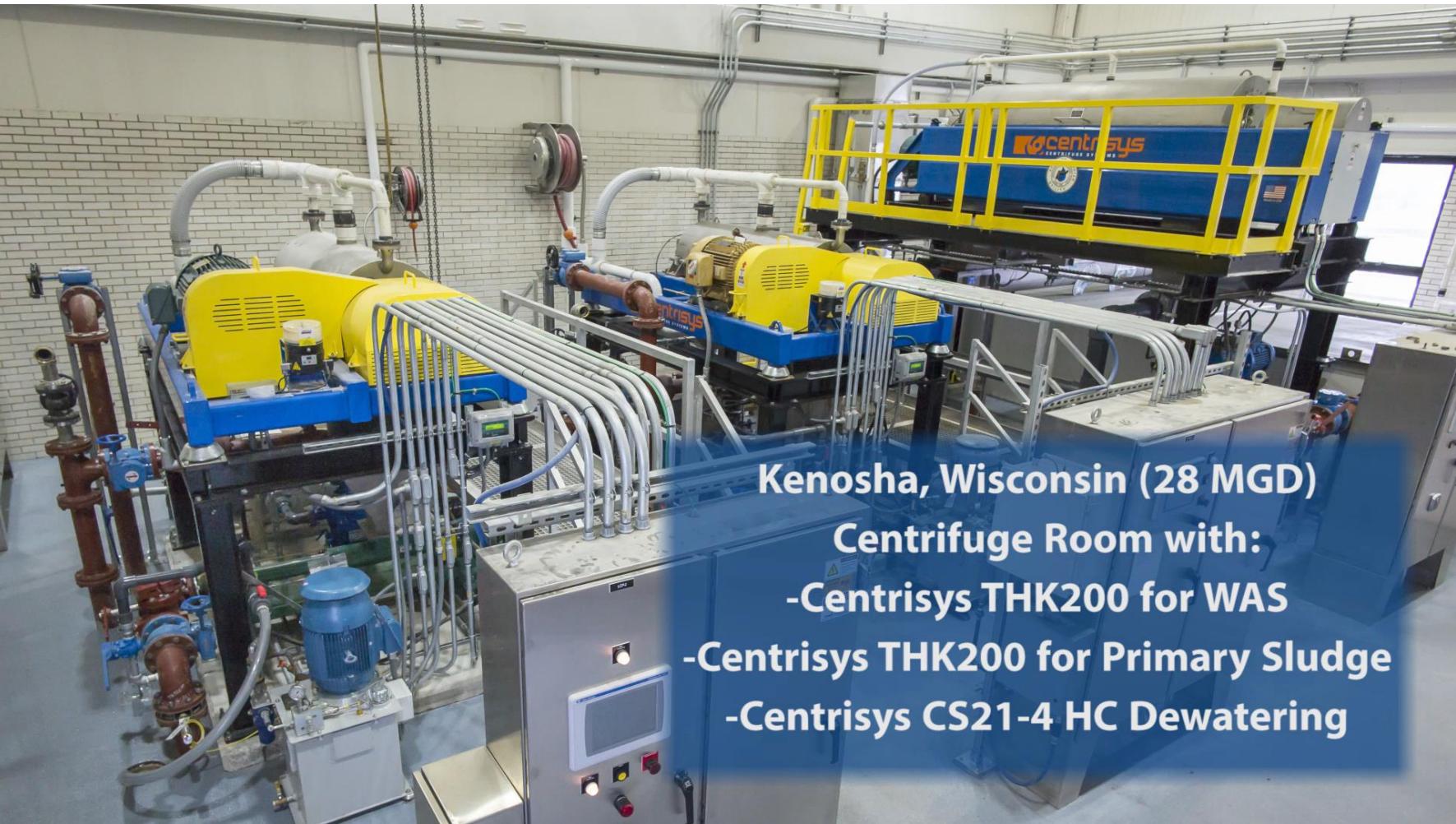
- ▶ Dewatering nearly constant (rd. 22 % solids)
- ▶ Reducing of the polymer consumption rd. 3 kg WS/ t TR, - 21 %

Process for thermal-chemical hydrolysis

**Reducing of the polymer consumption , Uelzen**



Process for thermal-chemical hydrolysis  
Gas production in Kenosha, USA in a break



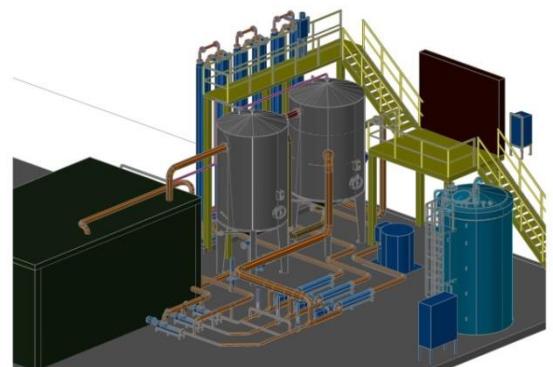
Process for thermal-chemical hydrolysis  
Reduction of the viscosity, Kenosha, Centrisys/CNP

# Nutrient reduction and recovery, Kalmar 2018

Ort	Durchsatz	EGW	Baujahr	Anmerkungen	Anlass
Kläranlage Gifhorn	2,2 m³/h	65.000	2005	24-h Betrieb	Nicht ausreichende Wärme vorhanden und überschäumende Faulung
Kläranlage Ratekau	2,0 m³/h	45.000	2007	Über Nacht Standby	Faulung überlastet
Kläranlage Nordhorn	2,5 m³/h	70.000	2013	Auch als Hygienisierung KAT 3 nutzbar	Faulung überlastet und geringe Mengen KAT3 Material
Kläranlage Köln-Stammheim	30 m³/h	1.500.000	2014	PONDUS nur Lizenzgeber, noch in der Optimierung	Besser Ausnutzung der Faulung
Kläranlage Uelzen	3,7 m³/h	80.000	2013	24-h Betrieb	Erhöhte Stromerzeugung und überlastete Faulung
Kläranlage Kenosha (USA)	5,6 m³/h	100.000	2014	24-h Betrieb	Erhöhte Gas- und Stromerzeugung bei gleichzeitiger Reduktion der betriebenen Faulbehälter
Kläranlage Wolfsburg	5,3 m³/h	135.000	2014/17	24-h Betrieb	Mehrgasproduktion für den Betrieb der Trocknung
Testanlage Kompetenzzentrum Berlin	15 l/h	2.000.000	2018	Fertiggestellt	Testanlage für den Schlamm aus Berlin Waßmannsdorf
Entsorgungszentrum Wuwei (VR China)	16,7 m³/h		2018/19	in Bau	Reduktion der Schlammmenge

für 2018: Löhne und Göppingen in Vorbereitung

Process for thermal-chemical hydrolysis  
Reference



## Plant in Wolfsburg

Design flow	5,3 m <sup>3</sup> /h
Heat power	370 kW
temperature	65 °C
Retention time 1.+2. Stufe	2,1 h

### 1. results:

start April 2017,  
With new digester

PO<sub>4</sub>-P 40 => 480 mg/l (total 960)

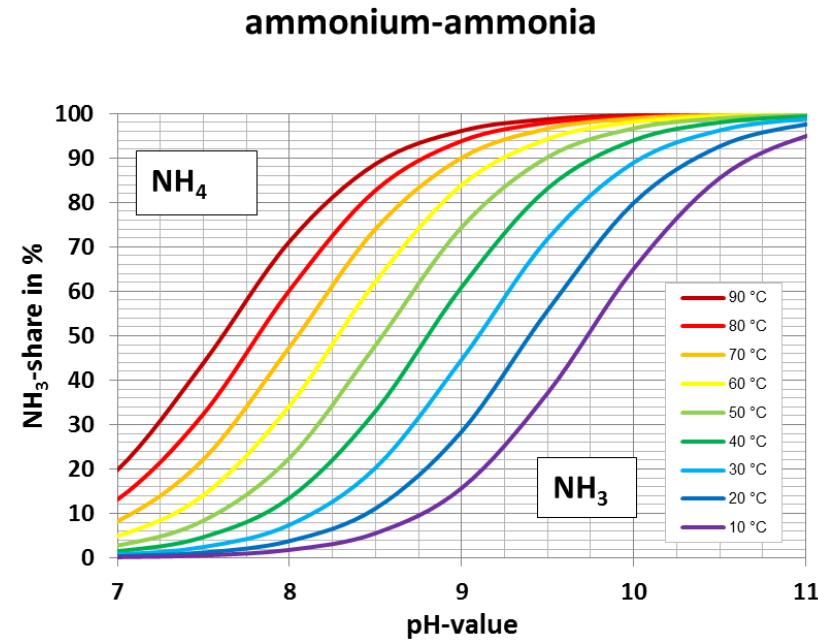
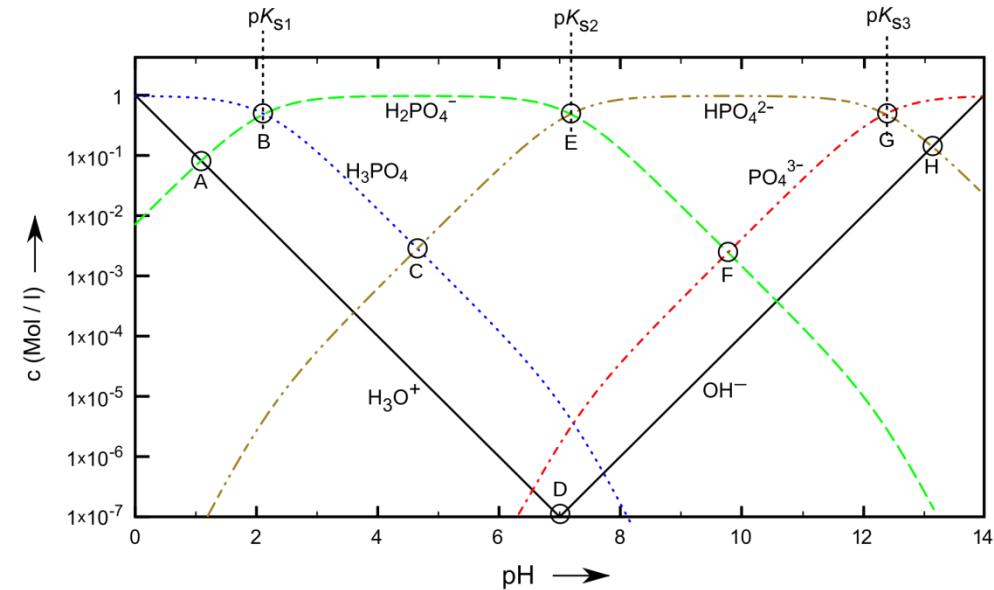
NH<sub>4</sub>-N 8 => 440 mg/l (total 3500)



Process for thermal-chemical hydrolysis  
**Release of phosphorus by hydrolysis**

# But phosphorus alone does not make happy, either

Can we also talk a little bit about nitrogen???



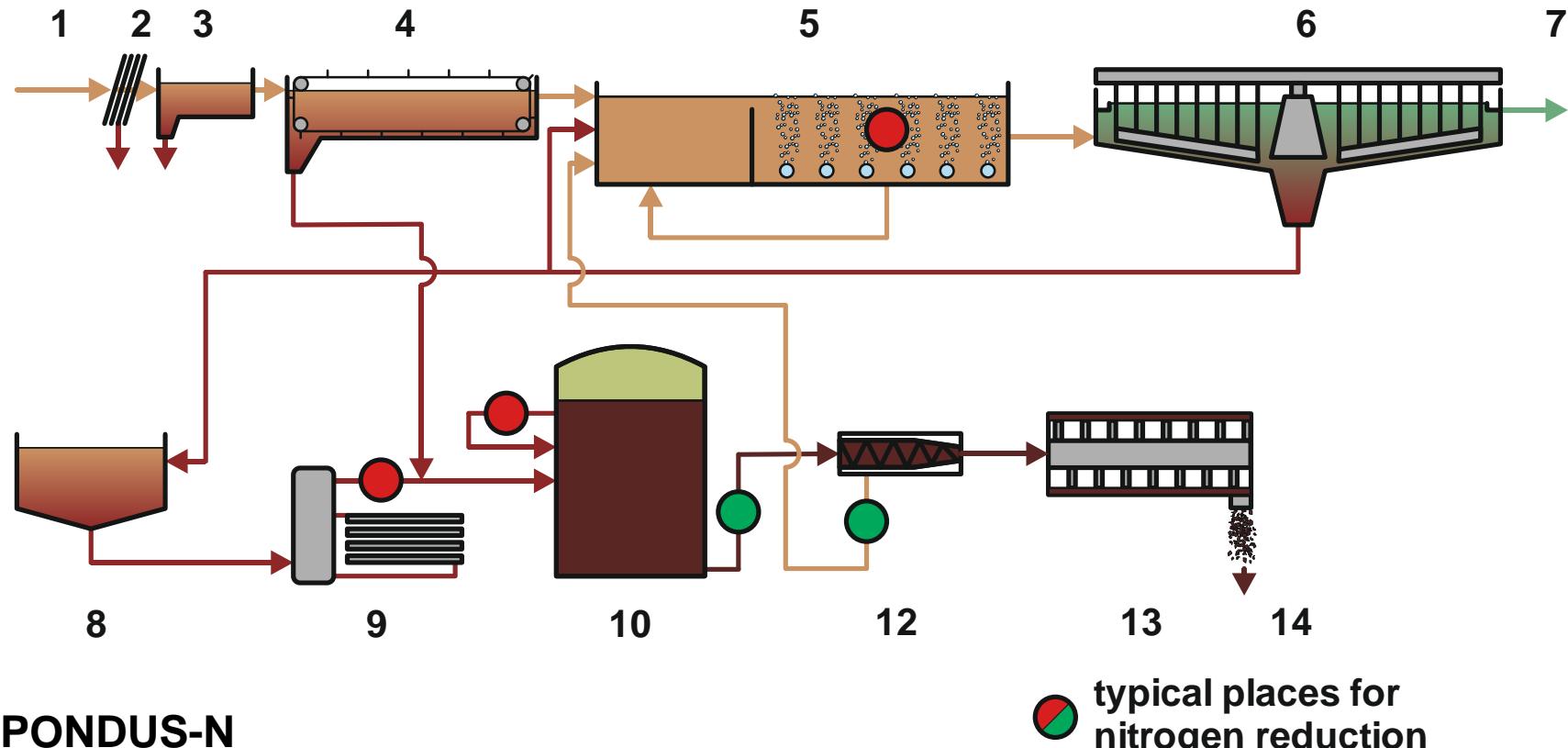
Which diagram is more beautiful ?

PONDUS-N

Everyone talks about phosphorus, the next is nitrogen

## A little trip to nitrogen,

## the PONDUS-N process



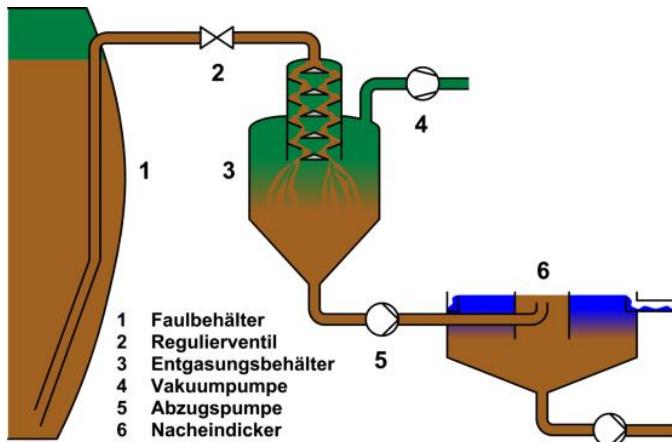
PONDUS-N

Typical places for nitrogen reduction

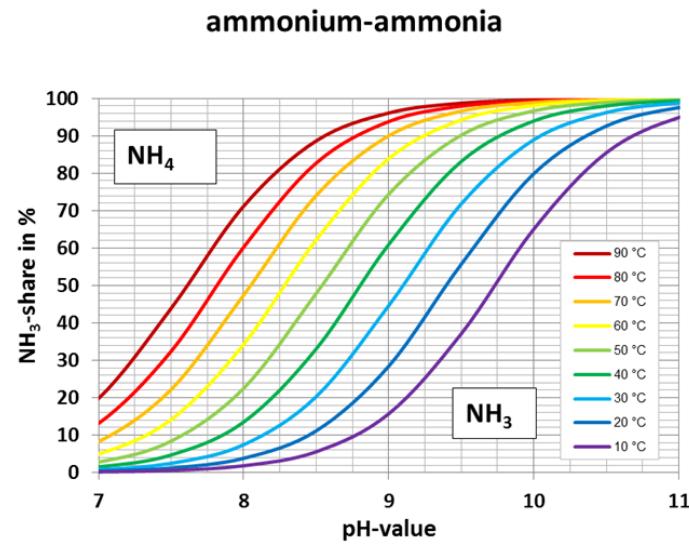


# PONDUS-N, a system for nitrogen recovery

Based on the proven  
sludge vacuum degassing



The chemical is typical



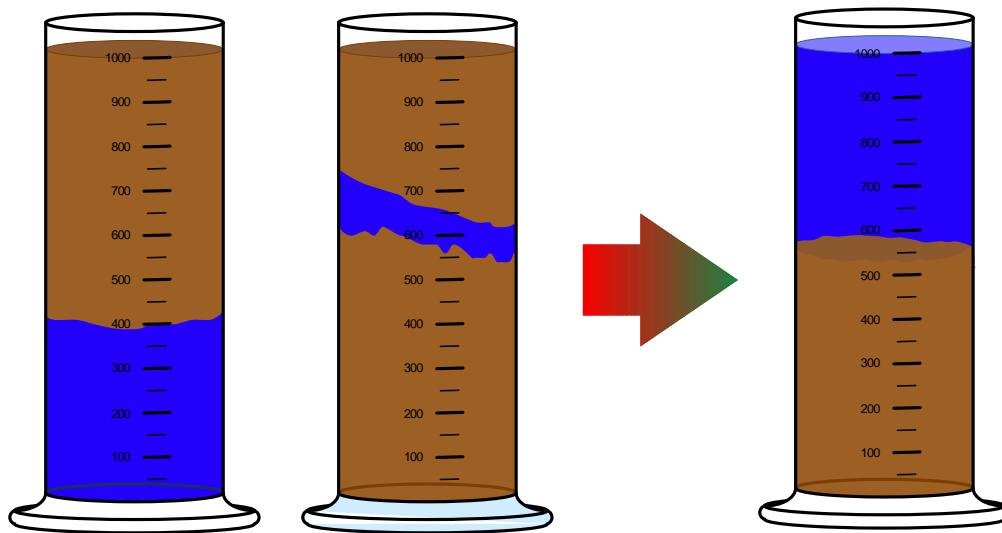
but the process is different

**PONDUS-N**  
The base of our system

# PONDUS-N, the base digested sludge degassing

The problem in  
the post thickener

Sedimentation of digested sludge



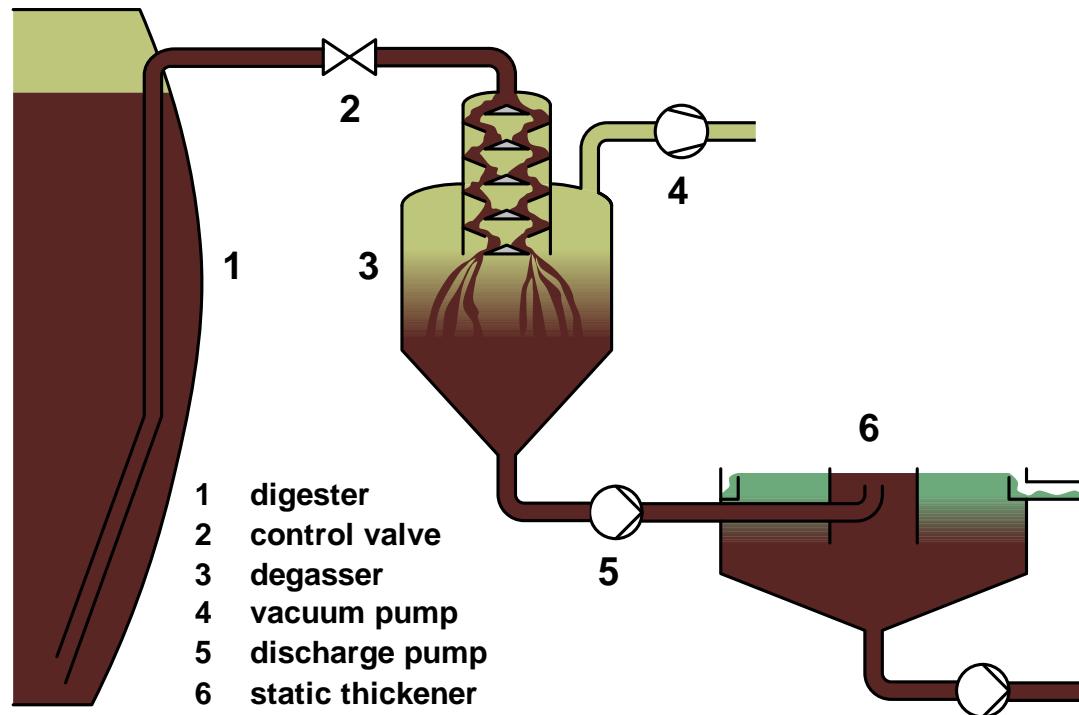
PONDUS-N

without degassing

with degassing

## The reason for digested sludge degassing

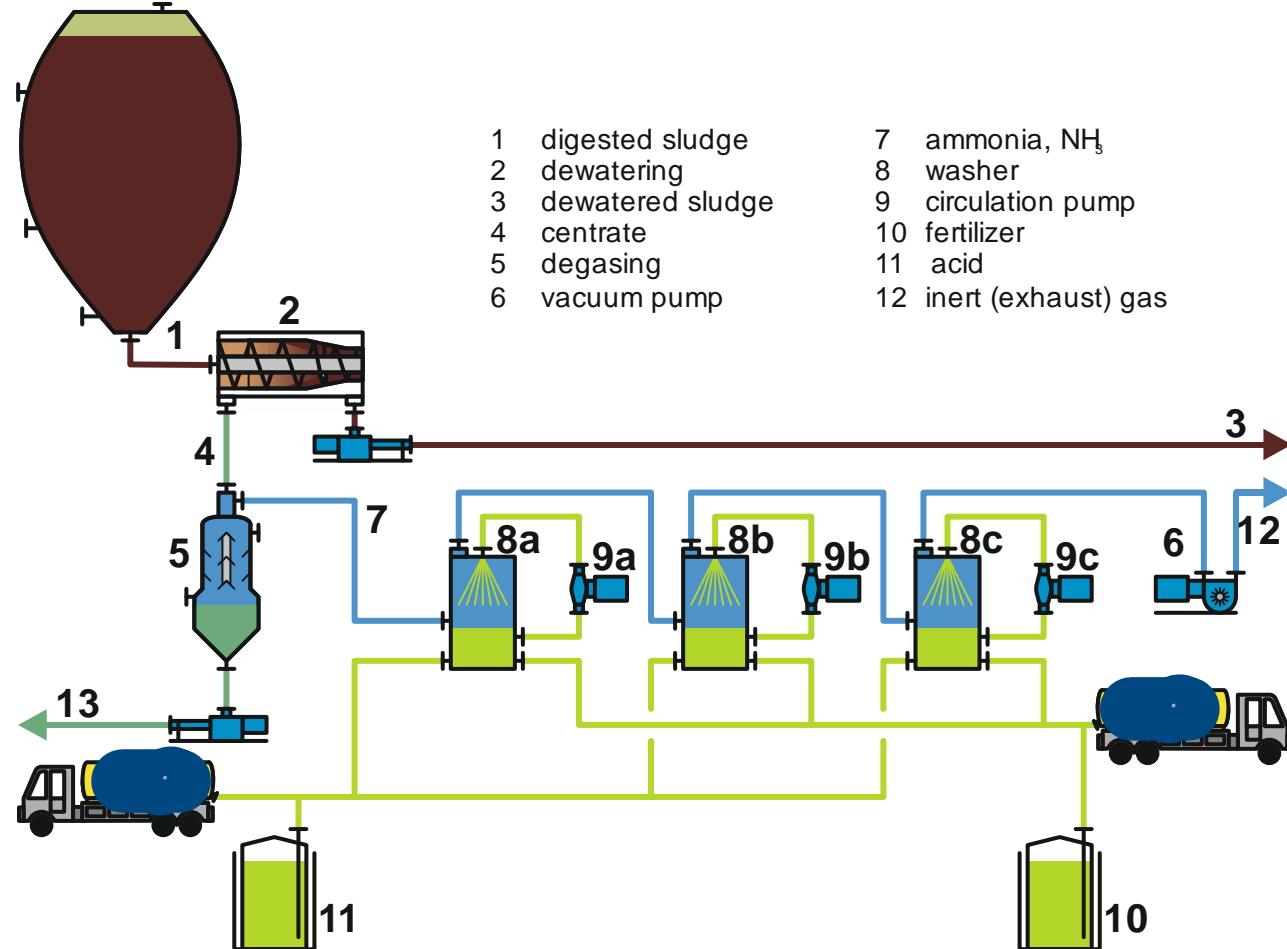
# PONDUS-N, the base process digested sludge vacuum degassing



**PONDUS-N**

## The process of digested sludge degassing

## The PONDUS–N process

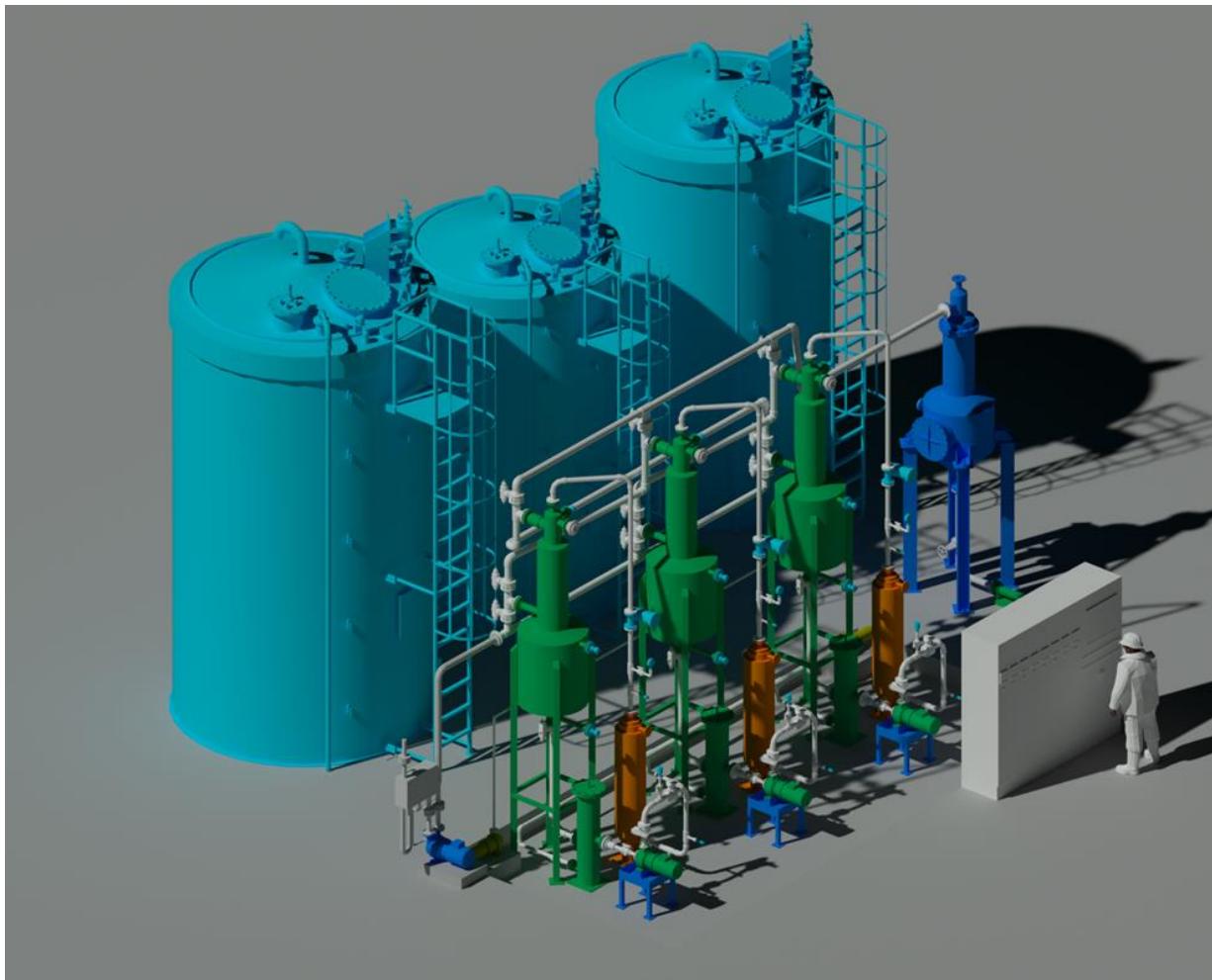


PONDUS-N

The process, example for water of dewatering

Nutrient reduction and recovery,  
Kalmar 2018

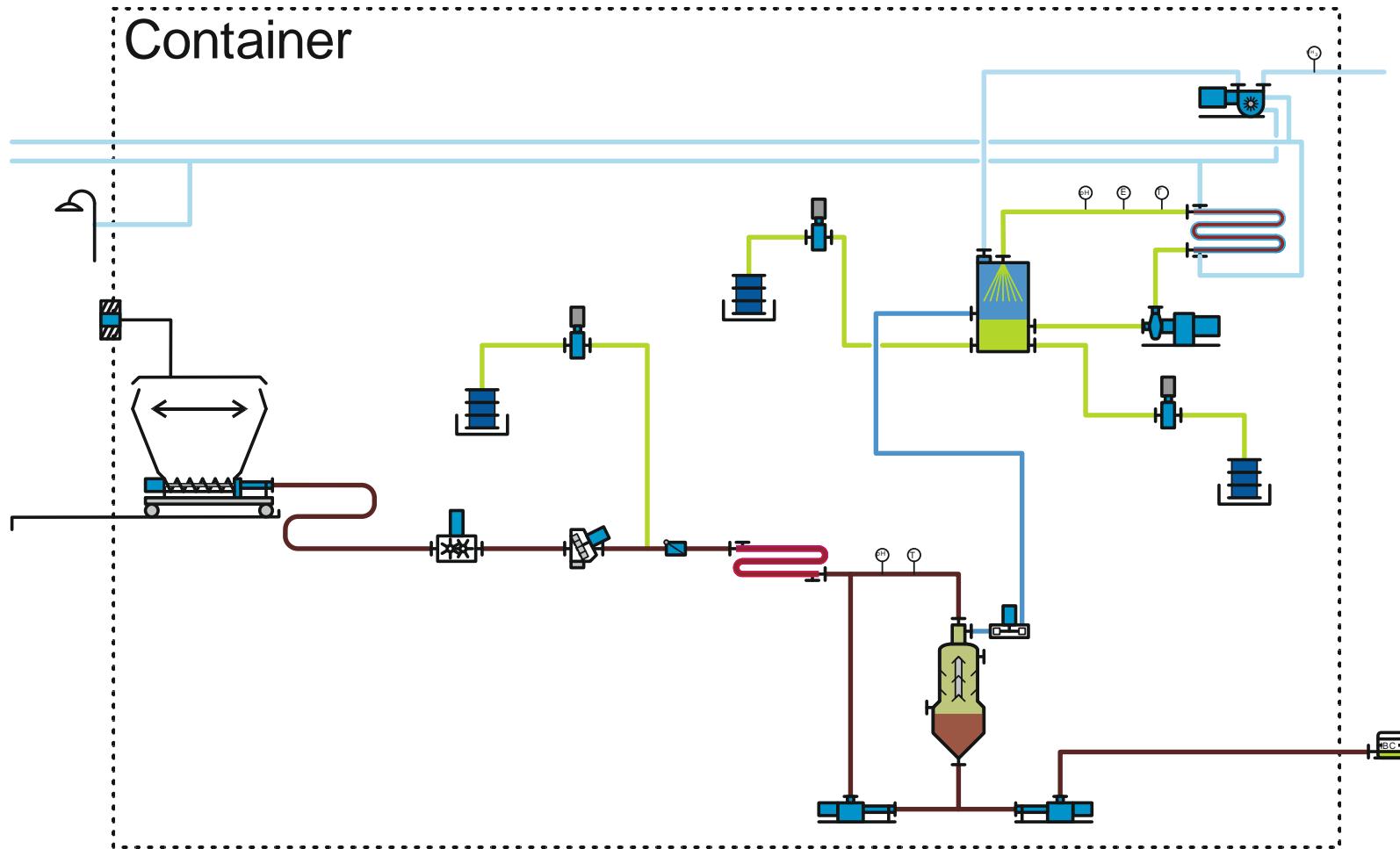
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**PONDUS-N**  
**Example for 300 T PE**

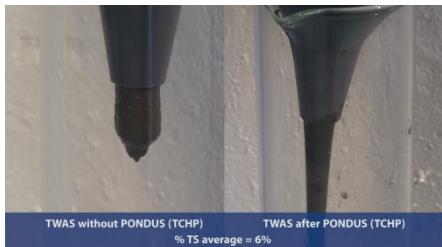
# Nutrient reduction and recovery, Kalmar 2018

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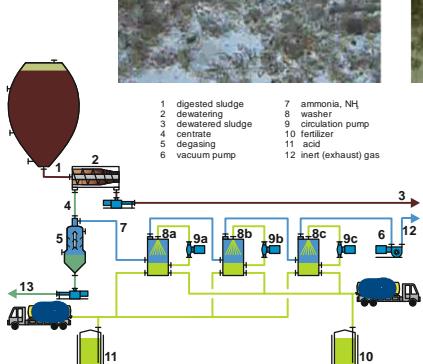
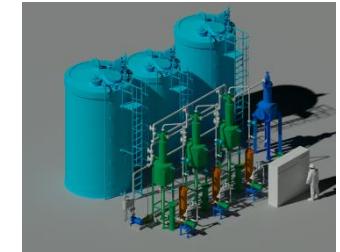
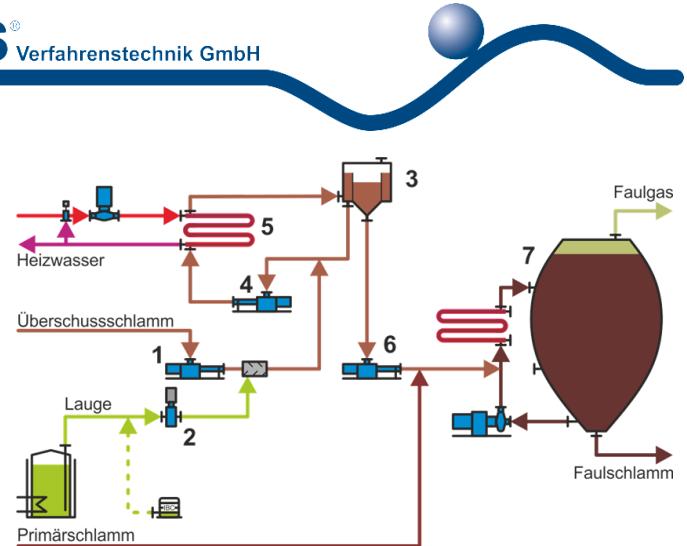


**PONDUS-N**  
**Pilot plant for HORIZON 2020**

# Nutrient reduction and recovery, Kalmar 2018



**Thank you for  
your patience**



**Thermal-chemical hydrolysis and PONDUS-N**